

Dear Author

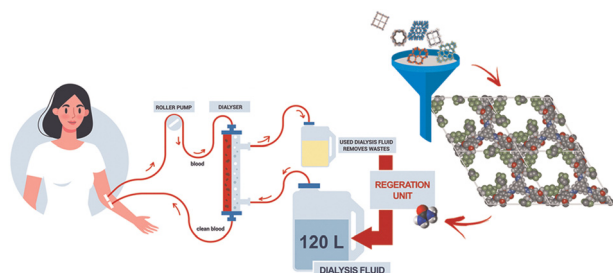
Please use this PDF proof to check the layout of your article. If you would like any changes to be made to the layout, you can leave instructions in the online proofing interface. First, return to the online proofing interface by clicking "Edit" at the top of the page, then insert a Comment in the relevant location. Making your changes directly in the online proofing interface is the quickest, easiest way to correct and submit your proof.

Please note that changes made to the article in the online proofing interface will be added to the article before publication, but are not reflected in this PDF proof.

If you would prefer to submit your corrections by annotating the PDF proof, please download and submit an annotatable PDF proof by clicking the button below.

 [Annotate PDF](#)

We have presented the graphical abstract image and text for your article below. This briefly summarises your work, and will be presented with your article online.



In silico screening of nanoporous materials for urea removal in hemodialysis applications

Thomas Fabiani, Eleonora Ricci, Cristiana Boi, Simone Dimartino and Maria Grazia De Angelis*

A molecular computational pipeline is designed to screen 560 porous crystals for urea removal from water to build a wearable artificial kidney. Calculations indicate that COFs functionalised with fluorine are the best candidates.

Please check this proof carefully. Our staff will not read it in detail after you have returned it.

Please send your corrections either as a copy of the proof PDF with electronic notes attached or as a list of corrections. **Do not edit the text within the PDF or send a revised manuscript** as we will not be able to apply your corrections. Corrections at this stage should be minor and not involve extensive changes.

Proof corrections must be returned as a single set of corrections, approved by all co-authors. No further corrections can be made after you have submitted your proof corrections as we will publish your article online as soon as possible after they are received.

Please ensure that:

- The spelling and format of all author names and affiliations are checked carefully. You can check how we have identified the authors' first and last names in the researcher information table on the next page. **Names will be indexed and cited as shown on the proof, so these must be correct.**
- Any funding bodies have been acknowledged appropriately and included both in the paper and in the funder information table on the next page.
- All of the editor's queries are answered.
- Any necessary attachments, such as updated images or ESI files, are provided.

Translation errors can occur during conversion to typesetting systems so you need to read the whole proof. In particular please check tables, equations, numerical data, figures and graphics, and references carefully.

Please return your **final** corrections, where possible within **48 hours** of receipt following the instructions in the proof notification email. If you require more time, please notify us by email to pccp@rsc.org.

Funding information

Providing accurate funding information will enable us to help you comply with your funders' reporting mandates. Clear acknowledgement of funder support is an important consideration in funding evaluation and can increase your chances of securing funding in the future.

We work closely with Crossref to make your research discoverable through the Funding Data search tool (<http://search.crossref.org/funding>). Funding Data provides a reliable way to track the impact of the work that funders support. Accurate funder information will also help us (i) identify articles that are mandated to be deposited in **PubMed Central (PMC)** and deposit these on your behalf, and (ii) identify articles funded as part of the **CHORUS** initiative and display the Accepted Manuscript on our web site after an embargo period of 12 months.

Further information can be found on our webpage (<http://rsc.li/funding-info>).

What we do with funding information

We have combined the information you gave us on submission with the information in your acknowledgements. This will help ensure the funding information is as complete as possible and matches funders listed in the Crossref Funder Registry.

If a funding organisation you included in your acknowledgements or on submission of your article is not currently listed in the registry it will not appear in the table on this page. We can only deposit data if funders are already listed in the Crossref Funder Registry, but we will pass all funding information on to Crossref so that additional funders can be included in future.

Please check your funding information

The table below contains the information we will share with Crossref so that your article can be found *via* the Funding Data search tool. **Please check that the funder names and grant numbers in the table are correct and indicate if any changes are necessary to the Acknowledgements text.**

Funder name	Funder's main country of origin	Funder ID (for RSC use only)	Award/grant number
Kidney Research UK	United Kingdom	501100000291	Unassigned

Researcher information

Please check that the researcher information in the table below is correct, including the spelling and formatting of all author names, and that the authors' first, middle and last names have been correctly identified. **Names will be indexed and cited as shown on the proof, so these must be correct.**

If any authors have ORCID or ResearcherID details that are not listed below, please provide these with your proof corrections. Please ensure that the ORCID and ResearcherID details listed below have been assigned to the correct author. Authors should have their own unique ORCID iD and should not use another researcher's, as errors will delay publication.

Please also update your account on our online [manuscript submission system](#) to add your ORCID details, which will then be automatically included in all future submissions. See [here](#) for step-by-step instructions and more information on author identifiers.

First (given) and middle name(s)	Last (family) name(s)	ResearcherID	ORCID iD
Thomas	Fabiani		
Eleonora	Ricci		0000-0002-2479-3653
Cristiana	Boi	I-5454-2012	
Simone	Dimartino	I-3392-2012	0000-0002-9695-1278
Maria Grazia	De Angelis		0000-0002-1435-4251

Queries for the attention of the authors

Journal: PCCP

Paper: **d3cp01510f**

Title: ***In silico* screening of nanoporous materials for urea removal in hemodialysis applications**

For your information: You can cite this article before you receive notification of the page numbers by using the following format: (authors), Phys. Chem. Chem. Phys., (year), DOI: 10.1039/d3cp01510f.

Editor's queries are marked on your proof like this **Q1**, **Q2**, etc. and for your convenience line numbers are indicated like this 5, 10, 15, ...

Please ensure that all queries are answered when returning your proof corrections so that publication of your article is not delayed.

Query reference	Query	Remarks
Q1	Have all of the author names been spelled and formatted correctly? Names will be indexed and cited as shown on the proof, so these must be correct. No late corrections can be made.	
Q2	Have all of the funders of your work been fully and accurately acknowledged? If not, please ensure you make appropriate changes to the Acknowledgements text.	

In silico screening of nanoporous materials for urea removal in hemodialysis applications†

Thomas Fabiani,^a Eleonora Ricci,^{ib} ‡^b Cristiana Boi,^b Simone Dimartino^{ib} ^c and Maria Grazia De Angelis^{ib} *^a

Cite this: DOI: 10.1039/d3cp01510f

The design of miniaturized hemodialysis devices, such as wearable artificial kidneys, requires regeneration of the dialysate stream to remove uremic toxins from water. Adsorption has the potential to capture such molecules, but conventional adsorbents have low urea/water selectivity. In this work, we performed a comprehensive computational study of 560 porous crystalline adsorbents comprising mainly covalent organic frameworks (COFs), as well as some siliceous zeolites, metal organic frameworks (MOFs) and graphitic materials. An initial screening using Widom insertion method assessed the excess chemical potential at infinite dilution for water and urea at 310 K, providing information on the strength and selectivity of urea adsorption. From such analysis it was observed that urea adsorption and urea/water selectivity increased strongly with fluorine content in COFs, while other compositional or structural parameters did not correlate with material performance. Two COFs, namely COF-F6 and Tf-DHzDPr were explored further through Molecular Dynamics simulations. The results agree with those of the Widom method and allow to identify the urea binding sites, the contribution of electrostatic and van der Waals interactions, and the position of preferential urea–urea and urea–framework interactions. This study paves the way for a well-informed experimental campaign and accelerates the development of novel sorbents for urea removal, ultimately advancing on the path to achieve wearable artificial kidneys.

Received 3rd April 2023,
Accepted 23rd August 2023

DOI: 10.1039/d3cp01510f

rsc.li/pccp

Introduction

Hemodialysis replaces kidney functionality by removing uremic toxins (UTs), rebalancing electrolytes and draining excess fluid. The technology relies on the extracorporeal exchange of compounds in the blood stream through a semipermeable membrane with a buffered solution called dialysate. Traditionally, HD is administered in hospital, in 4–5 hours sessions, two or three times a week;¹ due to the discontinuous treatment, the patient is subject to fluctuating concentrations of toxins and fluid accumulation, resulting in severe vascular and post-treatment stress. These drawbacks are a serious concern, especially for patients with comorbidities (*e.g.* cardiovascular

disease or diabetes), which are generally associated with chronic kidney disease (CKD).²

A significant improvement in the patient's lifestyle and health could come from home dialysis or through a wearable device. The biggest challenge lies in the downsizing of the water supply unit for which dialysis water needs to be purified and recirculated. In fact, after HD the spent dialysate contains the UTs removed from the blood stream, mostly low molecular weight compounds such as urea, creatinine, uric acid and others.³ Urea is the hardest compound to be removed from the spent dialysate, due to its similarity with water, as the two molecules have similar size and are both polar and weakly nucleophilic. Furthermore, urea has a very low concentration in the dialysate;^{3–5} with reference values in many experimental works ranging between 2 and 41 mM.^{6–12} For this reason, the removal of urea from aqueous solutions, as a proxy for spent dialysate fluid, has been investigated by many research groups.^{13–15}

A dialysate regeneration unit that rebalances ions and captures uremic toxins could solve this problem, enable the design of a wearable artificial kidney (WAK)¹⁴ and reduce the water consumed in the process. Attempts at such portable systems have mostly been based on the concept of enzymatic decomposition of urea, using immobilised urease, such as in the REDY[®], a commercial device based on a multi-cartridge

^a Institute for Materials and Processes, School of Engineering, University of Edinburgh, Sanderson Building, Robert Stevenson Road, EH9 3FB, Edinburgh, Scotland, UK. E-mail: grazia.deangelis@ed.ac.uk

^b Department of Civil, Chemical, Environmental and Materials Engineering, University of Bologna, Via Terracini 28, 40131 Bologna (BO), Italy

^c Institute for Bioengineering, School of Engineering, University of Edinburgh, King's Buildings Colin Maclaurin Road, EH9 3DW, Edinburgh, Scotland, UK

† Electronic supplementary information (ESI) available: SL_screening. See DOI: <https://doi.org/10.1039/d3cp01510f>

‡ Current address: National Centre for Scientific Research “Demokritos”, Athens, Greece.

1 system.¹⁶ Urea was converted by urease into ammonium and
 carbon dioxide, activated carbon was used to capture uremic
 toxins such as creatinine, uric acid and part of the urea, while
 ion exchangers served to capture and rebalance the ammonium
 ions and CO₂ in the dialysate. Due to safety issues related to
 leaching of aluminium ions, REDY[®] was withdrawn from the
 market. Subsequent portable prototypes followed a similar
 concept of urea decomposition (e.g. the WAK[™], NeoKidney,
 AWAK, Dharma[™], Medtronic, Fresenius), using different sup-
 ports for urease or other designs, but only few of them reached
 the clinical trials so far.¹ Other devices relied on electro-
 oxidation of urea, but the formation of by-products, such as
 nitrogen oxides (NO₃⁻, NO₂⁻), ammonia (NH₃), chloramines
 and active chlorine species, is still an open issue.¹⁷

15 A technology based solely on an adsorption mechanism and
 without chemical reactions would be intrinsically free of by-
 products generation and thus safer. Indeed, many studies
 focused on the removal of urea from diluted solution, such as
 dialysate, using adsorption on nanoporous materials, as acti-
 vated carbon (AC), zeolites, metal organic frameworks (MOFs)
 or inorganic nanosheets, the most relevant results reported in
 Table 1. A discussion of the literature on the adsorption of urea
 on porous particles is beyond the scope of this article, as there
 are several reviews dealing with this topic.^{13–15} Based on a back-
 of the envelope calculation, the ideal sorbent should have a
 urea binding capacity of 100 mg g⁻¹ for a light wearable device,
 which could remove the daily urea production with 250 g of
 sorbent. Such a goal still represents a challenge for the materi-
 als tested so far.

30 Computational tools offer the possibility of testing condi-
 tions and materials that would require an extensive experi-
 mental campaign. Erucar *et al.* performed a computational
 screening focusing on bio-MOFs for the separation of
 UTs,^{18,19} showing that structures based on adenine, dicyana-
 mide and methionine could outperform conventional materials
 such as AC or zeolites. A similar approach was used to select six
 out of 354 MOFs with high uptake of indoxyl sulphate, a
 protein-bound UT.²⁰

40 Covalent organic frameworks (COFs) are based on covalently
 bound organic building blocks. The stability of COFs in water
 under extreme conditions of temperature and pH has been
 demonstrated experimentally.²¹ COFs represent an interesting
 class of nanoporous materials to be simulated at the molecular

level. The enormous number of combinations of ligands and
 functionalisations allow a free design of nano-cavities with the
 desired size and chemical environment. Furthermore, the
 structure of new hypothetical COFs, which have not yet been
 synthesised, can be generated through an *in silico* assembly of
 rigid blocks.²² This would allow a much broader computational
 screening, enabling the design of materials with specific prop-
 erties and advancing the understanding of the behaviour of
 COFs.²³ Despite these features, to the best of our knowledge,
 only a few works have focused on molecular simulations of
 COFs for UTs sorption, and they refer to the sorption of urea on
 single COF monolayers, which differ from the nanoporous
 structures object of the present study. Others examined creati-
 nine and uric acid adsorption on ACA-COF, but no experi-
 mental work has tested COFs for urea removal.^{24,25}

The present work aims to evaluate and classify nanostruc-
 tured materials for the selective adsorption of urea, with a focus
 on COFs. Similar approaches have been attempted to evaluate
 the performance of large COF libraries for gas separations.^{26,27}
 No experimental data on urea removal are available for this
 class of materials, therefore it is believed that a well-informed
 experimental campaign of such a wide set of materials should
 start with molecular screening rather than with random,
 expensive, and time-consuming tests. Other materials are also
 considered in this analysis, such as graphites, siliceous zeolites
 and metal organic frameworks (MOFs) for a total of 560 porous
 crystals.

A preliminary screening is carried out with the fast Widom
 insertion method to evaluate the interaction energies between
 individual sorbate molecules (urea or water) and the crystal
 frameworks. Such analysis allows to classify materials accord-
 ing to preferential interactions for urea over water, in relation
 to their pore diameter, surface area and elemental composi-
 tion. Based on these results, two structures were selected and
 analysed more in detail with molecular dynamics (MD) at
 different urea concentrations.

Methods

Database selection

The database selected comprised 26 zeolites, 34 graphite sheets
 and single wall carbon nanotubes (SWCNs), 433 COFs, and 67
 MOFs or COFs coordinating a transition metal. The latter

Table 1 Experimental static adsorption urea capacity of nanoporous materials.¹ PS nanoparticles ninhydrin groups rely on a chemical reaction of urea with functional groups

		Urea binding capacity (mg g ⁻¹)	Urea equilibrium concentration (mM)	Ref.	
50	Activated carbon	Amorphous carbon	8.8	10	19
	Silicalite (MFI)	Zeolite	28.97	8.6	8
	Mordenite (MOR)	Zeolite	2.49	8.6	8
	ZSM-5 (Si/Al ratio 400)	Zeolite	6.36	20	41
	ZSM-5 (Si/Al ratio 400)	Zeolite	6.63	10	42
	PS nanoparticles ninhydrin groups ¹	Functional polymer	126	20	12
	MXene (Ti ₃ C ₂ Tx)	Inorganic nanosheets	13.8	20	6,7
55	MoS ₂ with widened interlayer spacing	Inorganic nanosheets	63.9	2.3	43
	Cu-BTC	MOF	128	2	44

1 materials were treated separately from the other COFs, as the
2 presence of a metal could cause potential issues in biomedical
3 application, such as hemodialysis.

4 For zeolites, a subset of the database provided by the
5 International Zeolite Association (IZA) was used as a bench-
6 mark, as these structures were tested in the literature.⁸ The 26
7 frameworks (AHT, EON, ERI, ESV, EUO, FAU, FER, ITE, IWV,
8 LTJ, MEL, MFI, MON, MOR, MSE, MSO, MTT, MTW, MVY,
9 NES, NSI, PTY, SFS, TON, VFI) are zeolites with high silica
10 content (Si/Al ratio > 10), with few or devoid of acid sites. The
11 choice was made because experimental evidence showed that
12 hydrophobic zeolites were those with better performance in
13 urea capture.²⁸ In fact, the removal of aluminium from the
14 structure through acid treatment is commonly performed to
15 augment the hydrophobicity of the framework.²⁸ Moreover, the
16 presence of aluminium is a concern for its potential release in
17 the patient's blood stream. The structures chosen may be
18 modelled without any cation pairing or substitution of Si
19 atoms, *i.e.* as purely siliceous structures.

20 Graphite sheets, graphite square channels and SWCNs (34
21 structures) present in the RASPA database²⁹ were used as a
22 benchmark for modelling of nanoporous materials with high
23 hydrophobicity.

24 Although MOFs were not the main focus of this work due to
25 their instability in water, we included them in the database,
26 together with COFs coordinating a transition metal as a refer-
27 ence to consider the impact of transition metals in the struc-
28 ture. The list of MOFs studied is reported in the ESI.† Finally,
29 433 COFs from CoreCOF database²⁶ were considered, excluding
30 all structures containing boron (namely those based on borox-
31 ine, borazine and boronic ester) for their susceptibility to
32 hydrolysis in water and for low stability in the final application.

Simulation conditions

35 Pore size and available surface area of the frameworks were
36 calculated with Zeo++ version 0.3³⁰ by using a probe with a 1.4 Å
37 radius, compatible with a water molecule. Crystal frameworks
38 and penetrant molecules were considered to be rigid, as
39 motivated by the limited degrees of freedom of the crystal
40 structures and of the small adsorbates molecules without
41 rotatable bonds. In fact, COFs are based on building blocks
42 based on aromatic rings, lacking flexibility, favouring the
43 stacking during the synthesis. Therefore, the energy functional
44 form collapses to the inter-molecular contribution alone,
45 according to eqn (S1) (ESI†). Lennard Jones 12–6 (LJ) and Ewald
46 electrostatic potential were used to model the non-bonded
47 interactions. The van der Waals (VdW) and charge–charge
48 cut-off values was set to 12 Å. Lorentz–Berthelot mixing rule
49 was used. Crystals were parametrized by using the DREIDING
50 force field³¹ and assigning partial charge by EQeq method,³² as
51 reported in Section S1 (ESI†). For zeolites, fixed partial charges
52 were assigned to Si and O (Si = +2.05 and O = –1.025) according
53 to the results described in literature³³ since the EQeq imple-
54 mented in RASPA failed to produce a parametrization in
55 accordance with literature. The TIP5P-E model parameters were
56 used for the calculation of water excess chemical potential, as

such model proved to be superior in predicting the water
adsorption in zeolites.^{34,35} Urea was modelled as a rigid mole-
cule (Table S1, ESI†) using the parameters obtained by Weer-
asinghe and Smith to match the behaviour of urea in water
solution.^{36,37}

The excess chemical potential μ^{ex} was calculated through the
Widom insertion method^{38,39} in RASPA,^{29,40} according to
eqn (1).

$$\mu^{\text{ex}} = -k_{\text{B}}T \ln \int \langle \exp(-\beta \Delta U) \rangle_{N, s_{N+1}} d s_{N+1} \quad (1)$$

in which k_{B} is the Boltzmann constant and T the absolute
temperature. The variation in potential energy of the nanopor-
ous crystal after the insertion of a penetrant molecule in the
empty lattice, ΔU , is averaged over the configuration space of N
+ 1-particles system s_{N+1} . 30 000 insertions were performed in
each simulation at random positions. The simulations were
carried out probing the individual molecules (urea and water)
in the empty framework. The excess chemical potential μ^{ex}
represents the average binding energy of molecule i with the
framework, at infinite dilution. Free energy profiles were cal-
culated with RASPA as the projection of μ^{ex} calculated through
Widom method along each crystallographic dimension, with
the toolkit provided in the suite^{29,40}

The Henry's law constants $K_{\text{H},i}$ can be computed from μ_i^{ex} as:

$$K_{\text{H},i} = \frac{1}{RT\rho_{\text{f}}} \ln \left(\frac{\Delta \mu_i^{\text{ex}}}{RT} \right) \quad (2)$$

in which R is the universal gas constant and ρ_{f} is the framework
density. Water is the main competitor for binding of water-
soluble toxins such as urea, as explained above. For this reason,
we define an ideal selectivity as the difference $\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}}$,
equivalent to the ratio between the Henry's constant for urea
 $K_{\text{H,u}}$ and for water $K_{\text{H,w}}$ in logarithmic scale (eqn (3)).

$$\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}} = RT \ln \left(\frac{K_{\text{H,u}}}{K_{\text{H,w}}} \right) \quad (3)$$

The calculation of infinite dilution excess chemical poten-
tials required only 1.69 ± 1.3 h per molecule and structure.
After this fast screening, two selected COF structures (COF-F6
and Tf-DHzDPr) were studied through MD simulations, carried
out in RASPA. Urea molecules (1, 10, 100) were initially placed
randomly in the framework, reaching an equilibrium position
at the end of the simulation. Such loadings of urea correspond
to, respectively, 0.53, 5.3 and 53 mg g⁻¹ in COF-F6 and 0.73, 7.3
and 73 mg g⁻¹ in Tf-DHzDPr. Simulation boxes were built to
guarantee a minimum box side length of twice the cut-off for
both COF-F6 ($2 \times 2 \times 12$, 48 unit cells, $174 \times 123 \text{ \AA}^3$) and Tf-
DHzDPr ($2 \times 2 \times 18$, 78 unit cells, $185 \times 169 \text{ \AA}^3$) with a similar
total volume. Each canonical ensemble, with constant number
of molecules, volume and temperature (NVT), was simulated for
500 ps with 1000 cycles for initialization and up to 500 ps until
equilibration was observed, with a time step to 0.5 fs. Nose-
Hoover thermostat was used to keep temperature at 310 K (time
scale parameter 0.15 ps). Two trajectories were analysed for
each condition. Radial distribution functions $g(r)$ were

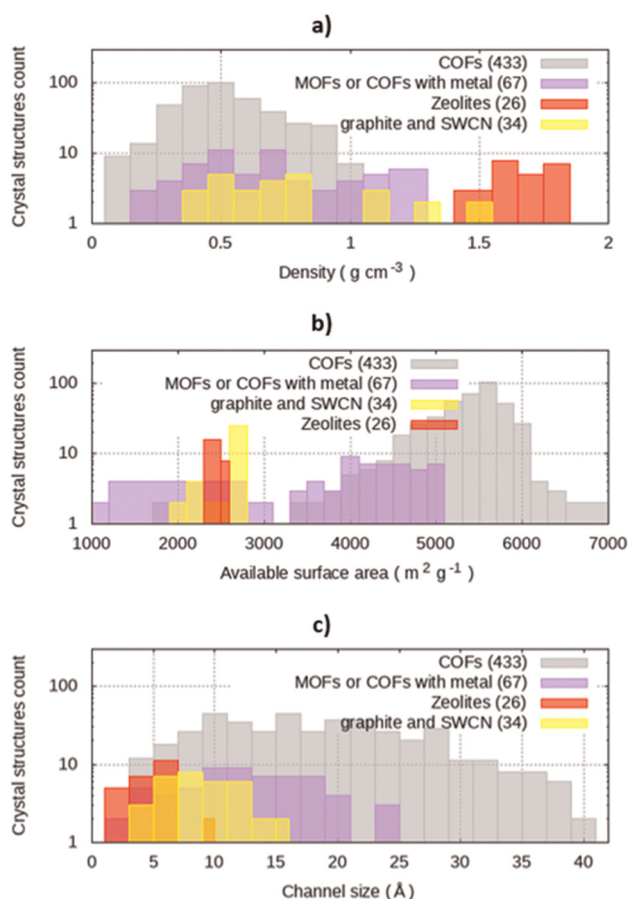
1 calculated in RASPA with the toolkit provided in the suite.^{29,40}
 All simulations were run on Precision 5820 Tower XCTO Base
 (Intel Core i9-10980XE 3.0 GHz, 4.8 GHz Turbo, 18C, 24.75 MB
 Cache, HT).

Results and discussion

Database analysis and description

10 The dataset used in our analysis was designed to study the
 COFs available on repositories, using other classes of materials
 as a reference. In the whole dataset of nanoporous crystals,
 densities range from 0.10 g cm^{-3} to 2.09 g cm^{-3} , with a median
 value of 0.58 g cm^{-3} (Fig. 1(a)). In particular, zeolites have
 density comprised between 1.33 and 2.09 g cm^{-3} with a median
 15 1.72 g cm^{-3} . The graphites and SWCNs present a scattered
 distribution of densities, ranging from 0.38 g cm^{-3} to 1.79 g cm^{-3} .
 COFs have a lower density with respect to zeolites, with a
 median density equal to 0.56 g cm^{-3} .

Surface area is a key parameter for the application, repre-
 20 senting the area available for adsorption, and it is reported in
 Fig. 1(b). The calculated available surface areas of zeolites,
 graphite, and SWCN are in the left side of the histogram, while



55 Fig. 1 Distribution of (a) density (g cm^{-3}), (b) available surface area ($\text{m}^2 \text{g}^{-1}$) and (c) channel size (\AA) on the database. The number between parentheses in the legend represents the number of structures included in every class.

COFs have larger values of surface per gram of materials. For
 instance, zeolites surface areas range between $2185 \text{ m}^2 \text{g}^{-1}$ and
 $2685 \text{ m}^2 \text{g}^{-1}$ with median value $2541 \text{ m}^2 \text{g}^{-1}$, while COFs has a
 median surface area of $5529 \text{ m}^2 \text{g}^{-1}$, with a standard deviation
 of $664.6 \text{ m}^2 \text{g}^{-1}$.

The calculated channel sizes ranges from 3.0 \AA to 11.2 \AA
 (median 6.2 \AA) for zeolites, while carbon-based materials have a
 broader distribution (between 5.1 and 16.7 \AA , median 9.9 \AA).
 For graphite sheets and graphite square channels, pore size
 calculations with Zeo++ agree with the structural features of the
 materials, namely the interlamellar distance for graphite sheets
 and the channel size for graphite square channels. (Fig. S1,
 ESI†). The whole database spans from 3.0 \AA up to 60.8 \AA , in the
 case of COF-122-2. Conversely from the other materials, with a
 limited span of pore size, COFs cover the whole range of pore
 sizes of the dataset, with a median value of 18.5 \AA (Fig. 1(c)),
 confirming the aforementioned tunability of pore size.

Urea and water excess chemical potential at infinite dilution

For most of the materials considered, and in particular for
 COFs, no experimental data on urea removal capacity are
 available to verify, even if only qualitatively, the simulation
 results. The only two data available in literature for the materi-
 als considered refer to two zeolites, silicalite (MFI) ($\text{Si/Al} \infty$) and
 mordenite (MOR) (Si/Al equal to 10). Such sorbents experimen-
 tally adsorb 28.97 mg g^{-1} and 2.49 mg g^{-1} of urea from a
 solution of 8.6 mM , respectively.⁸ Other materials were tested
 experimentally for urea sorption and they are summarized in
 Table 1. Interestingly, Cu-BTU, a metal organic framework,
 showed an adsorption capacity higher than 100 mg g^{-1} , with a
 performance attributable to a chemisorption mechanism.
 Erucar *et al.*¹⁸ screened a set of Bio-MOFs for urea adsorption,
 following a similar protocol, but using a different model for
 urea. A comparison in term of $\mu_{\text{u}}^{\text{ex}}$ and $\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}}$, between two
 MOFs simulated in this work and the ones from the literature is
 reported in Table S2 (ESI†). The calculations of the materials
 density, channel pore size, available surface area, urea and
 water excess chemical potential are reported in the SI Excel files
 SI_COFs, SI_MOFs, SI_C-materials and SI_Zeolites.

The infinite dilution performance of the materials was
 evaluated with the Widom insertion method, considering the
 excess chemical potential of urea $\mu_{\text{u}}^{\text{ex}}$ as a measure for urea
 binding strength, and the difference between excess chemical
 potential of urea and water $\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}}$, as a measure of urea/water
 selectivity (Fig. 2). The bisecting line in Fig. 2 represents a
 condition in which interaction between framework and water is
 zero, since $\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}} = \mu_{\text{u}}^{\text{ex}}$.

Carbonaceous materials like graphites and SWCNs (yellow
 squares in Fig. 2) have no electronic polarization and they
 interact only through VdW forces with urea and water. The
 deviation from the bisecting line might be attributed to the
 VdW interactions with water. Furthermore, they lay roughly on
 a straight line, as the variation in interaction is purely given by
 structural reasons. Specifically, graphite sheets with the smal-
 lest inter-lamellar distance have the lowest value of $\mu_{\text{u}}^{\text{ex}}$ (-32.0
 kJ mol^{-1}) decreasing monotonically with increasing distance

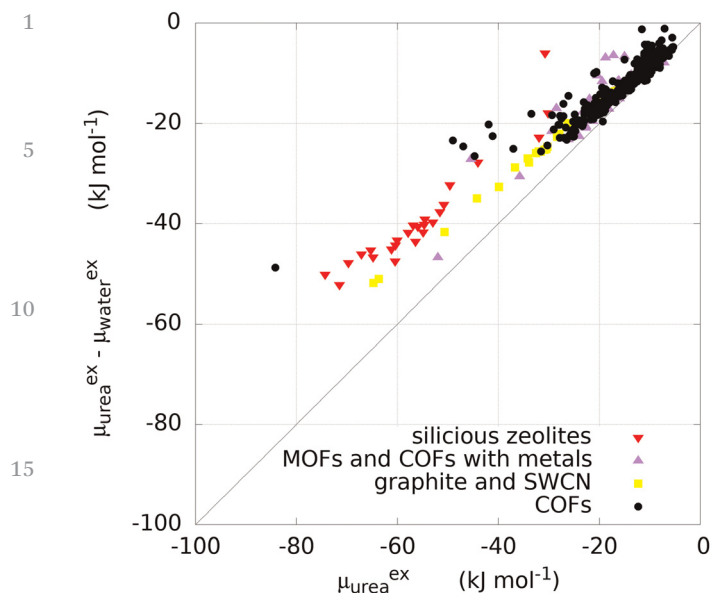


Fig. 2 Selectivity versus binding strength of purely siliceous zeolites (red down-pointing triangles), COFs (black circles), COFs containing a metal or MOFs (violet up-pointing triangles), graphite or SWCN (yellow squares).

between sheets (Fig. S2, ESI†). A similar trend was observed with graphite square channels, with lowest $\mu_{\text{u}}^{\text{ex}}$ of $-63.6 \text{ kJ mol}^{-1}$ for the structure with the smallest channel size. The monotonic trend may be explained by the fact that two layers of carbon atoms interact more with the urea molecule when lamellae are closer together.

The excess chemical potential of urea in zeolites (red triangles in Fig. 2) ranges between $-74.3 \text{ kJ mol}^{-1}$ (PTY) and $-30.15 \text{ kJ mol}^{-1}$ (-LTJ), with a median value of $-56.16 \text{ kJ mol}^{-1}$. One structure (MVY) shows a repulsive energy, due to the sieving effect related to the size of the pores, as small as 3.0 \AA (not shown in Fig. 2 and not included in the statistics). MOFs and COFs containing a transition metal (violet triangles in Fig. 2) do not show preferential binding of urea with respect to COFs (black circles in Fig. 2). Most COFs own a $\mu_{\text{u}}^{\text{ex}}$ not greater than

$22.96 \text{ kJ mol}^{-1}$ in absolute value but some of them show higher absolute values with a maximum of 84.2 kJ mol^{-1} .

The key features of the 12 COFs with highest absolute value of urea Excess Chemical Potential are reported in, while the complete list of values for all materials inspected is reported in the SI. These structures (Fig. S3, ESI†) have a channel diameter ranging from 4.1 \AA to 26.9 \AA and a broad distribution of surface area (2184 to $5932 \text{ m}^2 \text{ g}^{-1}$). On the chemical point of view, all of them contain highly electronegative atoms, such as fluorine, oxygen, nitrogen and sulphur. Interestingly, the top-5 COFs contain fluorine as a functional group, usually grafted as pre or post-synthetic modification of the linker. Each of the twelve contain nitrogen, as it is required for the building blocks reaction, and 9 of them have oxygen in their structure.

Interestingly, some of the structures reported in Table 2 have a corresponding COFs structure with a different linker functionality. For instance, COF-F6, synthesized to be a proton conductor, is based on the same linkers of Tf-DHz COFs⁵⁴ (Tf-DHzDPr-COF, Tf-DHzDAll-COF, Tf-DHzDM-COF, Tf-DHzDM-COF-1, Tf-DHzDAll-COF-1, Tf-DHzDAll-COF-2) with $\mu_{\text{u}}^{\text{ex}}$ ranging from -27.8 to -6.2 kJ mol^{-1} . In this series, the fluorination enhances dramatically the binding strength toward urea with respect to groups like propyl, allyloxy or methyl.

Following the same comparison between analogues, TpPa COFs family,^{47,55-58} based on ketoenamine linkage (TpPa-F₄, TpPa-NO₂, TpPa-SO₃H, TpPa-SO₃H-Py, TpPA-2, CCOF-TpPa-1, TpPa-(OH)₂, TpPa-Py, TpPa-1, TpPa-1-2F, TpPa-OMe₂ in increasing order according with their $\mu_{\text{u}}^{\text{ex}}$) show an important effect of the functionalization of the pore on the $\mu_{\text{u}}^{\text{ex}}$ ranging from -44.7 to -7.1 kJ mol^{-1} . Specifically, highly electronegative functionalization of the COF, such as fluorine, nitric, sulphonyl groups appears to promote the binding strength toward urea.

Similarly, the NUS family,^{48,59,60} based on ketoenamine linkage, have a trend of $\mu_{\text{u}}^{\text{ex}}$ according to heteroatoms on the structure increasing from -37.1 to -6.3 kJ mol^{-1} in the following order: NUS-3, NUS-10, NUS-50, NUS-9, NUS-51, NUS-2, NUS-15, NUS-14. Structures NUS-14 and NUS-15 contain only nitrogen as heteroatom, while NUS-2, NUS-3, NUS-50, NUS-51

Table 2 Features of the 12 COF frameworks with the lowest value of urea excess chemical potential and Tf-DHzDPr COF: density, pore size (as largest free sphere), available surface area (ASA), $\mu_{\text{u}}^{\text{ex}}$, $\mu_{\text{w}}^{\text{ex}}$ and $\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}}$ and elemental composition in oxygen, nitrogen and fluorine

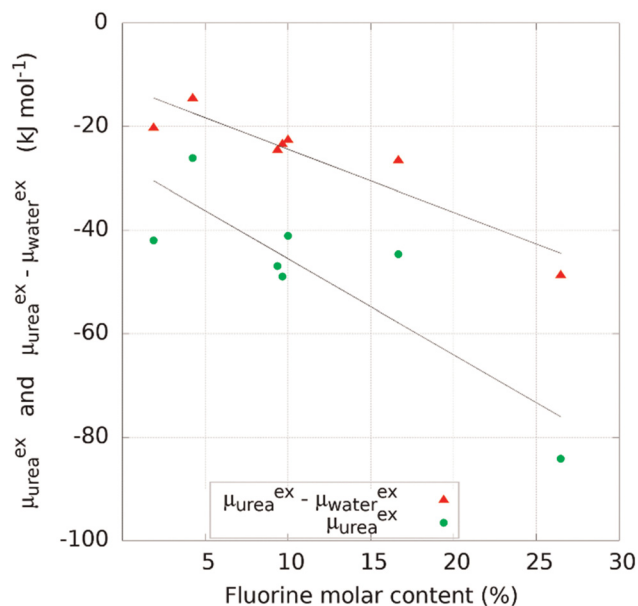
Framework name	Density g cm^{-3}	Pore size \AA	ASA $\text{m}^2 \text{ g}^{-1}$	$\mu_{\text{u}}^{\text{ex}}$ kJ mol^{-1}	$\mu_{\text{w}}^{\text{ex}}$ kJ mol^{-1}	$\mu_{\text{u}}^{\text{ex}} - \mu_{\text{w}}^{\text{ex}}$ kJ mol^{-1}	Oxygen content %	Nitrogen content %	Fluorine content %	Ref.
COF-F6	1.09	10.6	4568	-84.2	-35.4	-48.7	5.9	5.9	26.5	45
CF3-TFP-ITA	0.59	19.0	5102	-49.0	-25.6	-23.4	0.0	6.5	9.7	46
CF3-TFP-TAPB	0.52	19.4	5217	-47.0	-22.4	-24.6	0.0	3.1	9.4	46
TpPa-F4	1.02	14.9	3979	-44.7	-18.1	-26.6	8.3	8.3	16.7	47
COF-F	0.56	26.9	4851	-41.1	-18.6	-22.6	0.0	10.0	10.0	N/A
NUS-3	0.69	16.7	5090	-37.1	-12.0	-25.1	13.6	9.1	0.0	48
DAPH-TFP	0.54	23.5	5290	-33.4	-15.4	-18.1	5.9	11.8	0.0	49
NPN-1	1.05	4.1	4772	-31.5	-5.9	-25.6	8.2	8.2	0.0	50
PP-TzDa-AB	0.70	7.3	5932	-30.3	-5.9	-24.4	5.1	5.1	0.0	51
COF-318	1.14	13.0	2184	-29.0	-7.8	-21.2	14.3	7.1	0.0	52
COF-316	1.14	13.0	3091	-28.1	-7.8	-20.3	13.3	6.7	0.0	52
CCOF-6	0.89	5.7	5177	-27.9	-5.0	-22.9	6.8	3.4	0	53
Tf-DHzDPr-COF	0.74	15.8	5651	-27.8	-9.4	-18.5	8.0	8.0	0	55

1 contain also oxygen as hydroxyl, ketonic or ether groups. NUS-9 and NUS-10 have sulfonic groups in their structure.

2 Only few of the materials in this database were tested for separation purposes, for instance NUS-3 and NUS-2 were used
 5 in a MMM for CO₂ separation,⁴⁸ while CCOF-6 was synthesized to be used in chromatography of enantiomers. Other applications of the COFs in Table 2 are proton conduction, sensing or catalysis. Interestingly, most of the TpPa-COF,⁴⁷ as well as COF-318, COF-316,⁵² CF3-TFP-TAA, CF3-TFP-TAPB,⁴⁶ CCOF-6⁵³
 10 proved to be stability in boiling water and extreme acid and basic conditions, retaining their crystalline structure. Furthermore, all of them, excepting NPN-1, showed to retain their structure up to 300 °C during the thermogravimetric analysis. The 12 COFs were obtained through solvothermal synthesis, for instance COF-F6 was obtained after 3 days in 1,4-dioxane and mesitylene using acetic acid, as a catalyst, at 120 °C.⁴⁵ The entire list of values of μ_u^{ex} calculated is reported in the ESI† in the various spreadsheets.

20 Correlation of structure performance with elemental composition and structural parameters

25 Nitrogen content and oxygen content in COFs did not correlate with the excess chemical potential of urea, as reported in Fig. S4 (ESI†). The top 12 COF structures, in terms of excess chemical potential over urea, reported in Table 2, have molar nitrogen content between 3.2% and 11.8% and molar oxygen content as high as 14.3%. On the other hand, the fluorine content has a clear quantitative impact, as reported in Fig. 3, with the highest values recorded in COF-F6 containing 25% of F atoms. A similar trend is observed between the urea/water selectivity and fluorine content, with increasing selectivity as fluorine content increases.



55 Fig. 3 Effect of fluorine molar content on the urea binding and selectivity of COFs with fluorine atoms in the structure.

The excess chemical potential and urea/water selectivity of COF structures showed no clear correlation with pore size and available surface area (Fig. S5, ESI†). While these parameters are traditionally used for the description of nanoporous materials, the positioning, orientation, and quality of functional groups, as well as the intermolecular interactions formed upon adsorption of the urea/water species, are hardly described by pore size and available surface area. This highlights the need for more meaningful descriptors able to capture the properties of the crystalline structure and the chemical environment of the pore.

MD simulation of urea adsorption in COF-F6 and Tf-DHzDPr

The screening carried out through the chemical potential at infinite dilution showed the impact of functionalization on the COFs pores on the promotion of selective interaction toward urea. To highlight the role played by fluorine atoms, two COF materials, COF-F6 and Tf-DHzDPr-COF were comparatively investigated at higher loading through MD simulations.

COF-F6 is the best performing crystal in terms of urea binding strength at infinite dilution, while Tf-DHzDPr-COF, based on the same building blocks as COF-F6, has a propyl chain connected to the oxygen, instead of the fluorinated tail (see Fig. 4). In particular, COF-F6 and Tf-DHzDPr share the same node monomer (benzene-1,3,5-triyltrimethanol) and a similar linker; the former is based on 2,5-di-(6,6,6,5,5,4,4,3,3-nonafluoro-hexoxy)-terephthalohydrazide (Fig. 4(a)), while the latter uses the 2,5-dipropoxyterephthalohydrazide (Fig. 4(b)), differing from the chain attached to the aromatic ring. The resulting crystal structures are reported in Fig. 4(c) for COF-F6 and Fig. 4(d) for Tf-DHzDPr. The presence of a bulky functional group in COF-F6 results in a reduction of pore size and surface area with respect to Tf-DHzDPr, shifting from to 15.83 Å to 10.56 Å and from 5651 m² g⁻¹ to 4568 m² g⁻¹.

Simulations were carried out in the absence of water molecules as solvent for urea in the framework. In general, the simultaneous presence of both species would result in water molecules competing with urea for interactions with the adsorbent. At the same time, water partially hydrates urea in the bound states, providing favourable intermolecular stabilization of adsorbed urea molecules. The impact of water needs to be thoroughly investigated and will be the object of future study.

MD NVT simulations locate the equilibrium position of the urea molecule in the framework and to calculate the potential energy in that position. The excess chemical potential calculated through the Widom approach, on the other hand, evaluates the average value of the potential energy estimated at different random positions of one molecule in the crystal.

The equilibrium position of the urea molecule in the framework resulting from the MD simulation corresponds to the location of one of the free energy minima obtained with Widom mapping (Fig. 5), indicating the agreement of the two methodologies. Multiple minima are evidenced by MD runs and they refer to equivalent binding sites, due to the symmetry of the crystal structure. In particular, the MD simulation yields a potential energy of the system of $-115.0 \text{ kJ mol}^{-1}$ ($\pm 0.01\%$)

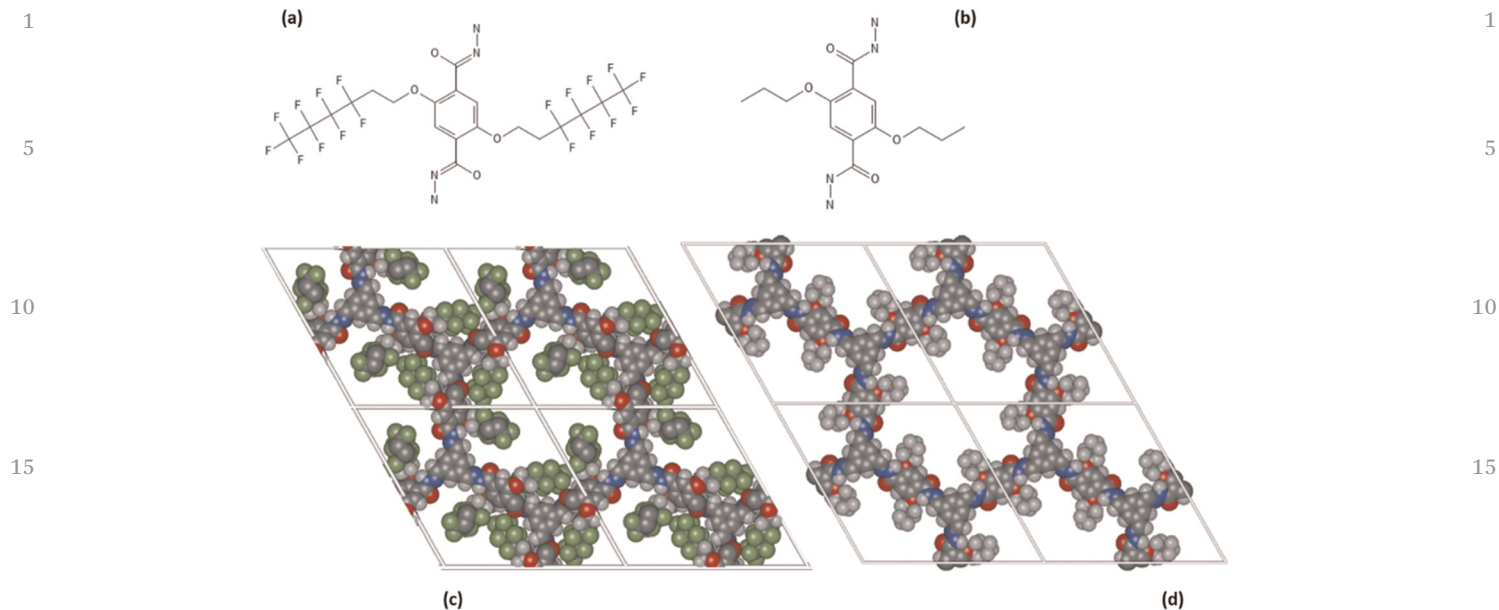


Fig. 4 (a) 2,5-di-(6,6,6,5,5,4,4,3,3-nonafluoro-hexoxy)-terephthalohydrazide, (b) 2,5-dipropoxyterephthalohydrazide, (c) Structure of COF-F6 (z-projection) (d) Structure of Tf-DHzDPr (z-projection).

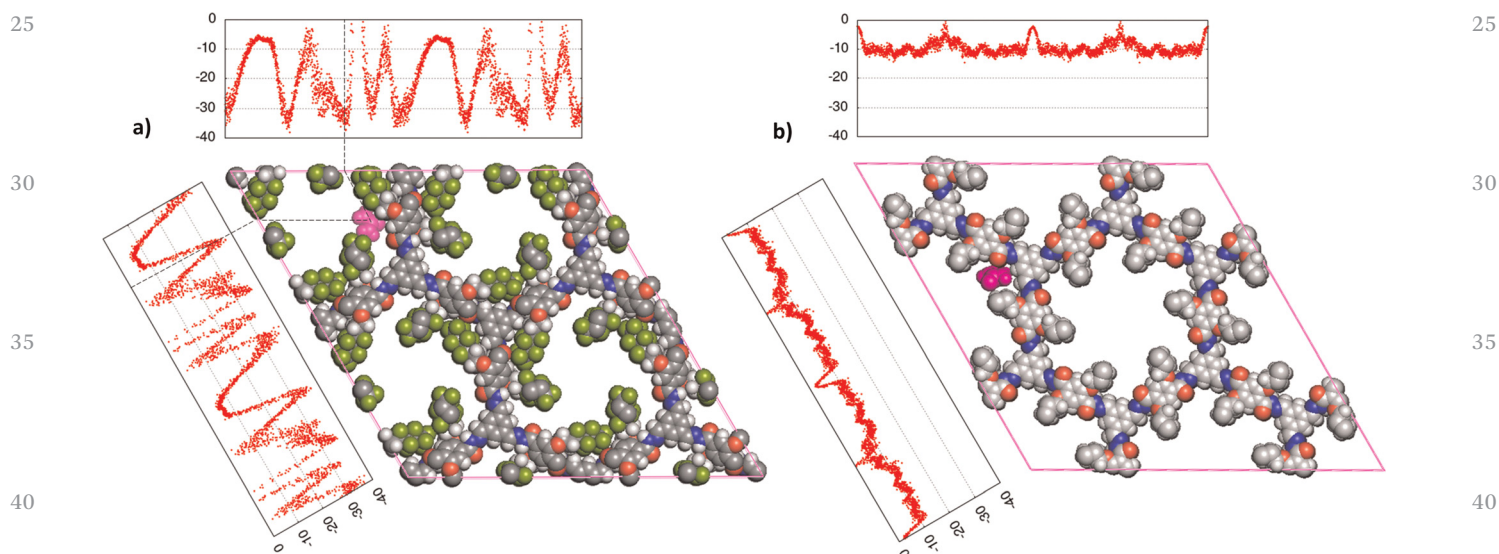


Fig. 5 Superposition of preferential binding site obtained by MD simulations (represented by the molecular structure, MD trajectory snapshot, area in purple) and the free energy profile over the two crystal dimensions (a) and (b) mapped by Widom insertion method, on Tf-DHzDPr. C atoms in the framework are grey, O atoms are in red, N atoms in blue, H atoms in white.

in COF-F6 and $-45.9 \text{ kJ mol}^{-1}$ ($\pm 0.50\%$) in Tf-DHzDPr, *versus* values of $-84.2 \text{ kJ mol}^{-1}$ and $-27.8 \text{ kJ mol}^{-1}$ evaluated with the Widom method. The difference is due to the fact that MD simulation evaluates the energy of the most favourable binding site, while the Widom insertion procedure averages the excess chemical potential over a uniform sampling of the unit cell, according to eqn (1). The sampling of Tf-DHzDPr with the insertion method provided an almost flat trend over the two directions of the unit cell (Fig. 5), with values mostly comprised between -5 kJ mol^{-1} and -15 kJ mol^{-1} . This difference

between the two materials may be addressed with the absence of strong polar centers in the Tf-DHzDPr defining preferential site in terms of position and orientation for the urea molecule.

The adsorption of a urea molecule in the nanoporous materials, at a given concentration in the bulk, requires chemical (together with thermal and mechanical) equilibrium. This condition implies the equality between the chemical potentials of urea in the external water solution and in the nanoporous materials. Kokubo *et al.* reported chemical potential for urea in a water solution, equal to $-85.57 \text{ kJ mol}^{-1}$

with the model used in this work, at a concentration of 42.86 mM (2.71 g L^{-1}), considered in many works as an upper bound for urea concentration in CKD patients' blood. Particularly, the excess chemical potential μ^{ex} is equal to $-41.31 \text{ kJ mol}^{-1}$ (with a contribution from van der Waals and electrostatic terms that are respectively 2.14 kJ mol^{-1} and $-46.40 \text{ kJ mol}^{-1}$). The ideal chemical potential, due to the urea concentration in water is equal to $-44.26 \text{ kJ mol}^{-1}$.³⁷

The infinite dilution chemical potential $\mu_{\text{u}}^{\text{ex}}$ calculated with the insertion method does not include the stabilization due to the partial solvation of water in the framework and the ideal contribution of the chemical potential, that are by definition negative. Nonetheless, urea in COF-F6, according to the Widom insertion method reaches a $\mu_{\text{u}}^{\text{ex}}$ equal to $-84.2 \text{ kJ mol}^{-1}$, showing the compatibility of binding strengths in COFs with the adsorption of urea at the concentration of interest.

To consider the effect of a larger number of urea molecules in the structure we designed systems for COF-F6 and Tf-DHzDPr, as explained in the methods sections. Upon increasing the number of molecules, a slight decrease of the absolute value of potential energy per molecule is observed for COF-F6, while Tf-DHzDPr displays a less definite trend.

Fig. 6 shows the different contributions to the total potential energies. The VdW interaction term is smaller for COF-F6 (less than 24%), while for Tf-DHzDPr it represents up to 54% of the total interactions between urea and the framework. Fluorine in

COF-F6 binds urea molecules primarily through electrostatic forces. The urea–urea interactions, also reported in Fig. 6, arise only when there are at least 100 molecules in the system. This is compatible with a progressive filling of the materials, with urea molecules occupying the most favourable binding sites first, and then opting for less favourable interactions on the framework. This concept is corroborated by the slight decrease of the average interaction of urea molecules with the framework and the increasing urea–urea intermolecular interactions. The urea–urea intermolecular interactions are, in both cases, mostly electrostatic.

Intermolecular interactions between 100 urea molecules in COF-F6 are repulsive, while for Tf-DHzDPr they are attractive. In the latter material, the loss in interaction between urea molecules and framework is compensated by attractive interactions of adsorbate molecules which increase with their concentration. The urea molecules distribution in the two materials can be seen in Fig. S6 and S7 (ESI†).

The effect of increasing urea loading on the resulting interactions can be also studied analysing the radial distribution functions (RDF), describing the pairwise distance between atoms in the system. Interestingly, all individual urea atoms preferentially interact with COF-F6 fluorine, oxygen and hydrogen atoms. For instance, as shown in Fig. 7, hydrogen atoms bound to nitrogen in the urea structure interact tightly with fluorine atoms in COF-F6 (shown by the peak at a distance of 2 \AA in Fig. 7(a)). The oxygen atom in the urea molecule seems to privilege the interaction with hydrogen in the COF-F6 structure (shown by the peak at a distance of 2.5 \AA in Fig. 7(c)). Thus, urea owns a preferential orientation while adsorbing, supporting the presence of a binding site on COF-F6 provided by both atoms of the bone structure (hydrogens) and the tails (fluorines). This is testified by the peaks' positions of RDFs (reported in Fig. S8, ESI†) between 2 \AA and 4 \AA , showing relative position of urea atoms with respect to the framework. On the other hand, nitrogen atoms in the framework appear to be more distant from urea with distances higher than 4 \AA . The quality and the distance between electronegative atoms of urea and of the framework support the classification of such interactions as hydrogen bonds, in which the urea nitrogen behaves as a hydrogen bonds' acceptor.

The interactions established by the urea N atoms with O atoms in the framework, at increasing number of urea molecules, are reported in Fig. 8. Introducing 1 and 10 molecules of urea in COF-F6, oxygen in the framework binds urea nitrogen atoms, testified by the broad peak at 3.70 \AA , with soft and wide shape. With 100 molecules, the first peak is slightly shifted increasing its height (with respect to the other peaks) and many peaks emerge between 2.5 and 10 \AA . This means that, increasing the number of molecules in the framework, urea starts to establish tighter interactions with O atoms therein.

In Tf-DHzDPr the behaviour is different, as the framework lacks electronegative atoms on the exposed propyl tail. In this case, urea binds through its amine groups with the oxygen available on the framework, forming hydrogen bonding, while the carbonyl group in urea interacts with hydrogens on the

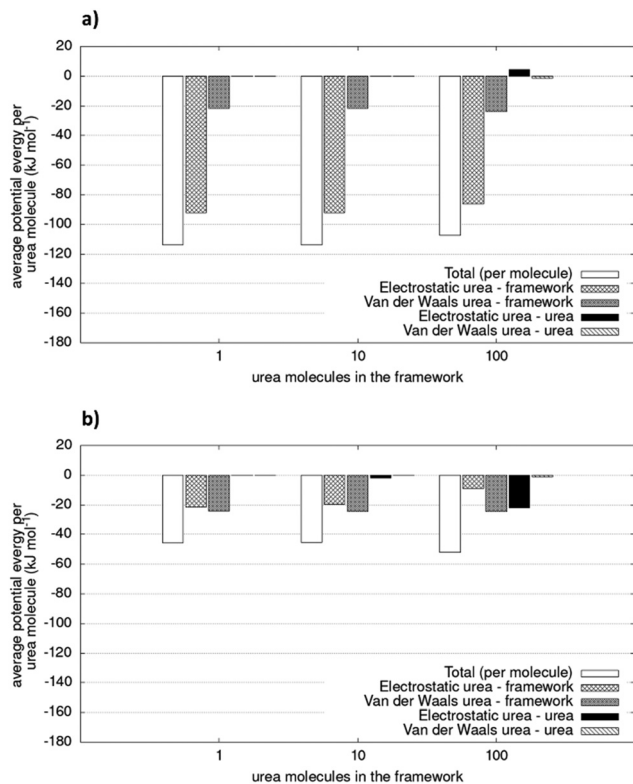


Fig. 6 Potential energy of simulated system (per urea molecule) for (a) COF-F6 and (b) Tf-DHzDPr. The values are average of two simulations. Relative errors of duplicate is lower than 1.2%.

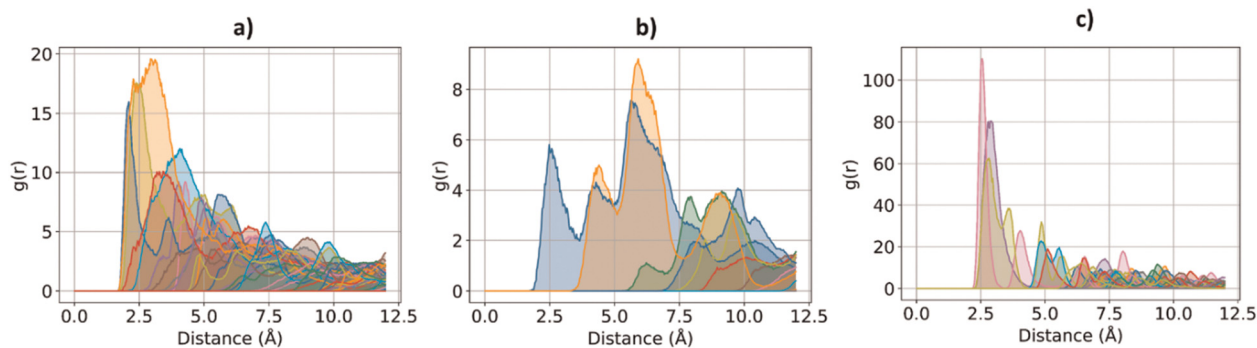


Fig. 7 RDF for the system of COF-F6 with 1 urea molecule: (a) urea H atoms with F atoms on COF-F6, in (b) urea H atoms with O atoms of COF-F6 and in (c) urea O atoms with H atoms of COF-F6.

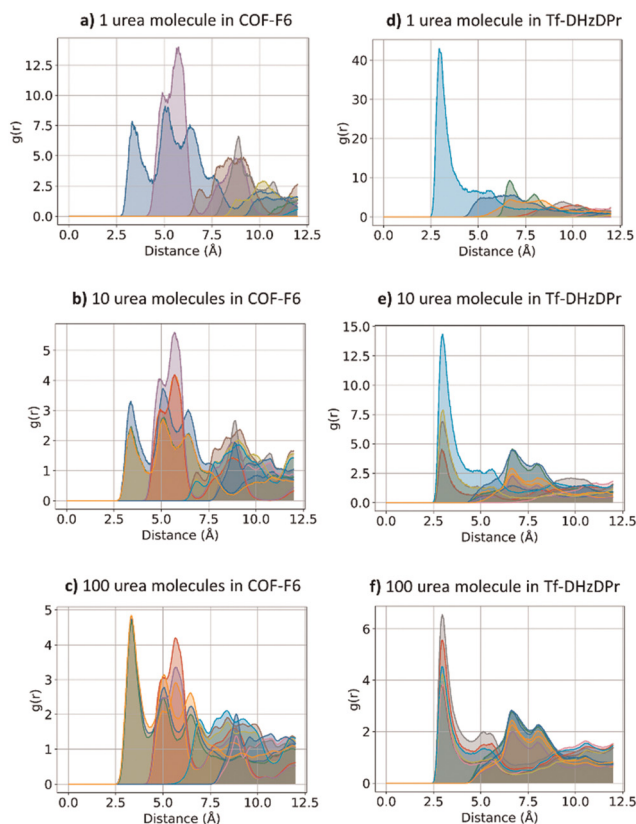
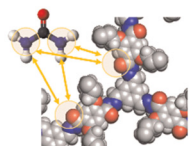


Fig. 8 RDF for urea N atom with respect to O atoms in the frameworks. COF-F6 with 1 molecule (a), 10 molecules in (b), 100 molecules in (c) and Tf-DHzDPr with 1 molecule (d), 10 molecules (in e), 100 molecules in (f). Each curve represents a different oxygen in the framework's structure.

framework surface. This is showed by the peaks' position in Fig. S8 (ESI[†]): in this case oxygen atoms play a prominent role in

binding urea, when only one molecule is placed in the framework. A sharp peak between 2.5 and 4 Å in the radial distribution function computed between oxygens of the sorbent, and hydrogens and nitrogens of the urea molecule confirms the previous statement. Even in this case, nitrogen atoms in the framework appear far from the urea molecules, in fact RDF with C atoms in urea do not show a peak closer than 4 Å. Also in Tf-DHzDPr, upon increasing the number of urea molecules, the RDF undergo a modification (Fig. 8). In this case, the peaks at closest distance remains unperturbed, with an increasing number of overlapping peaks at the same distance, due to the progressive filling of preferential binding locations. Conversely from COF-F6, additional peaks, overlapping or shifted at higher distance with respect to the others, appear with 100 molecules, showing the interaction of urea in other sites.

Therefore, COF-F6 and Tf-DHzDPr bind urea differently; the former has fluorine atoms providing strong electronegative sites that prevail over the other hydrogen bonding donors and acceptors on the structure. Multiple atoms of urea in these crystals interact with each other, arranging in order to minimize repulsion. Specifically, a concentration of 53 mg g⁻¹ in COF-F6 results in urea molecules interacting with each other, at a distance of 4.8 Å (Fig. S10, ESI[†]), but there is no specific relative orientation, confirming that the interaction with the framework is strong enough to compensate the energetic penalty of repulsion between urea molecules (Fig. 6). Such evidence agrees with the energetic contributions to the potential energy reported in Fig. 6. For Tf-DHzDPr at 73 mg g⁻¹ of urea in the framework, the molecules are 4.53 Å apart and they orient themselves to maximize their attraction. This is suggested by the defined peaks at 2.08 Å and 3.73 Å in Fig. 9(d), proof of an orientation of urea molecules while they are bound to the framework (oxygen atoms in urea are oriented toward hydrogen atoms of other urea molecules).

Although partial charge parametrisation showed to be a source of uncertainty in the reproduction of adsorption performance in organic frameworks,^{61,62} the chemical pore environment in COFs seems to strongly influence the urea binding strength, demonstrating their potential as sorbents for urea removal.

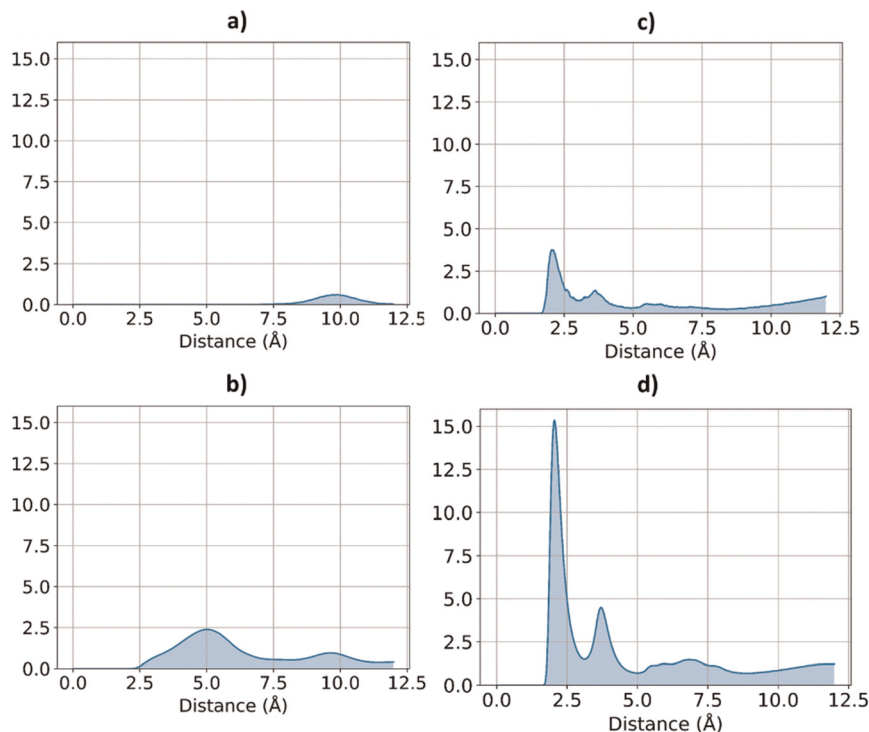


Fig. 9 RDF for urea O atoms and H urea atoms, in the two frameworks, at different concentration of urea. COF-F6 with 10 urea molecules (a) and 100 urea molecules in (b), Tf-DHzDP with 10 urea molecules in (c) and 100 urea molecules in (d).

However, functionalisation could reduce the pore space available for sorption, thus limiting the maximum theoretical amount of urea molecules in the system.

Conclusions

In this study, a database of 560 porous crystals containing zeolites, graphitic materials, MOFs and COFs was screened to assess their potential as urea adsorbents to regenerate dialysate. The focus was put on COF materials which can guarantee high stability in water and low safety issues. The Widom insertion approach for excess chemical potential at infinite dilution allowed to rank the frameworks according to their affinity and selectivity towards urea. Fluorine content in the COF structures promotes the adsorption of urea and favours urea/water selectivity, with the framework COF-F6 having the best performance. Other structural parameters (*e.g.* pore size, surface area, *etc.*) or composition of other elements were not correlated to urea removal performance.

The results are consistent with MD simulations carried on COF-F6 and its non-fluorinated equivalent, Tf-DHzDP. The analysis of the radial distribution functions allowed to understand that electronegative atoms, such as fluorine or nitrogen atoms in the framework structure are crucial in forming hydrogen bonds with the sorbate. However, fluorination reduces the pores volume and the maximum number of urea molecules that can be theoretically loaded in the framework.

In conclusion, the screening indicates that the large freedom in linkers' selection gives space for optimizing and tailoring the frameworks on the desired application.

Furthermore, the computational method here presented is suitable for a fast preliminary screening of large materials databases and consistent with longer MD simulations. Such procedure can be used to inform and shorten the experimental campaign and also to explore hypothetical structures, not yet synthesised, assisting the design of new materials with target performance. Future work will inspect the competitive effect of water on the urea removal performance of selected materials.

Author contributions

Thomas Fabiani: conceptualization, data curation, investigation, formal analysis, software, writing – original draft. Eleonora Ricci: supervision, writing – review & editing. Cristiana Boi: writing – review & editing. Simone Dimartino: writing – review & editing. Maria Grazia De Angelis: conceptualization, funding acquisition, supervision, writing – review & editing.

Conflicts of interest

There are no conflicts to declare.

Acknowledgements

This project was supported by Kidney Research UK and the RSE, through the programs Kidney Medtech Competition

1 Award 2022, RSE Saltire Facilitation Workshop Award 2021 (Funder reference number 1898), and the RSE Scottish Government SAPHIRE Grant: 2022 (Funder reference number 2816). The School of Engineering at the University of Edinburgh has supported the PhD scholarship of Mr Thomas Fabiani.

Q2

Notes and references

- 10 1 M. K. van Gelder, S. M. Mihaila, J. Jansen, M. Wester, M. C. Verhaar, J. A. Joles, D. Stamatialis, R. Masereeuw and K. G. F. Gerritsen, *Expert Rev. Med. Devices*, 2018, **15**, 323–336.
- 15 2 W. G. Couser, G. Remuzzi, S. Mendis and M. Tonelli, *Kidney Int.*, 2011, **80**, 1258–1270.
- 3 R. A. Pollock, G. Yu Gor, B. R. Walsh, J. Fry, I. T. Ghampson, Y. B. Melnichenko, H. Kaiser, W. J. DeSisto, M. C. Wheeler and B. G. Frederick, *J. Phys. Chem. C*, 2012, **116**, 22802–22814.
- 20 4 H. D. Lehmann, R. Marten and C. A. Gullberg, *Artif. Organs*, 1981, **5**, 278–285.
- 5 J. T. Olesberg, M. A. Arnold and M. J. Flanigan, *Clin. Chem.*, 2004, **50**, 175–181.
- 6 F. Meng, M. Seredych, C. Chen, V. Gura, S. Mikhalovsky, S. Sandeman, G. Ingavle, T. Ozulumba, L. Miao, B. Anasori and Y. Gogotsi, *ACS Nano*, 2018, **12**, 10518–10528.
- 25 7 Q. Zhao, M. Seredych, E. Precetti, C. E. Shuck, M. Harhay, R. Pang, C.-X. Shan and Y. Gogotsi, *ACS Nano*, 2020, **14**, 11787–11798.
- 30 8 V. Wernert, O. Schäfer, H. Ghobarkar and R. Denoyel, *Microporous Mesoporous Mater.*, 2005, **83**, 101–113.
- 9 M. N. Z. Abidin, P. S. Goh, A. F. Ismail, N. Said, M. H. D. Othman, H. Hasbullah, M. S. Abdullah, B. C. Ng, S. H. S. A. Kadir and F. Kamal, *Carbohydr. Polym.*, 2018, **201**, 257–263.
- 35 10 W.-K. Cheah, Y.-L. Sim and F.-Y. Yeoh, *Mater. Chem. Phys.*, 2016, **175**, 151–157.
- 11 C.-H. Ooi, W.-K. Cheah and F.-Y. Yeoh, *Adsorption*, 2019, **25**, 1169–1175.
- 40 12 I. Geremia, J. A. W. Jong, C. F. van Nostrum, W. E. Hennink, K. G. F. Gerritsen and D. Stamatialis, *Sep. Purif. Technol.*, 2021, **277**, 119408.
- 13 W.-K. Cheah, K. Ishikawa, R. Othman and F.-Y. Yeoh, *J. Biomed. Mater. Res., Part B*, 2017, **105**, 1232–1240.
- 45 14 Y. Ma, S. Li, M. Tonelli and L. D. Unsworth, *Microporous Mesoporous Mater.*, 2021, **319**, 111035.
- 15 C. Gao, Q. Zhang, Y. Yang, Y. Li and W. Lin, *Biomater. Res.*, 2022, **26**, 5.
- 16 M. Roberts, *Nephrology*, 1998, **4**, 275–278.
- 50 17 M. K. van Gelder, J. A. W. Jong, L. Folkertsma, Y. Guo, C. Blüchel, M. C. Verhaar, M. Odijk, C. F. Van Nostrum, W. E. Hennink and K. G. F. Gerritsen, *Biomaterials*, 2020, **234**, 119735.
- 18 B. Akkoca Palabiyik, M. Batyrow and I. Erucar, *Sep. Purif. Technol.*, 2022, **281**, 119852.
- 55 19 T. Yildiz and I. Erucar, *Chem. Eng. J.*, 2022, **431**, 134263.
- 20 B. Li, S. Gong, P. Cao, W. Gao, W. Zheng, W. Sun, X. Zhang and X. Wu, *Ind. Eng. Chem. Res.*, 2022, **61**, 6618–6627.
- 21 X. Huang, C. Sun and X. Feng, *Sci. China: Chem.*, 2020, **63**, 1367–1390.
- 22 F. Haase and B. V. Lotsch, *Chem. Soc. Rev.*, 2020, **49**, 8469–8500.
- 23 Y. Lan, X. Han, M. Tong, H. Huang, Q. Yang, D. Liu, X. Zhao and C. Zhong, *Nat. Commun.*, 2018, **9**, 5274.
- 24 A. M. Jahromi, M. Khedri, M. Ghasemi, S. Omrani, R. Maleki and N. Rezaei, *Sci. Rep.*, 2021, **11**, 12085.
- 25 T. Skorjanc, D. Shetty, F. Gándara, S. Pascal, N. Naleem, S. Abubakar, L. Ali, A. K. Mohammed, J. Raya, S. Kirmizialtin, O. Siri and A. Trabolsi, *ACS Appl. Mater. Interfaces*, 2022, **14**, 39293–39298.
- 26 M. Tong, Y. Lan, Q. Yang and C. Zhong, *Chem. Eng. Sci.*, 2017, **168**, 456–464.
- 27 C. Kessler, J. Eller, J. Gross and N. Hansen, *Microporous Mesoporous Mater.*, 2021, **324**, 111263.
- 28 H. L. Jamieson, H. Yin, A. Waller, A. Khosravi and M. L. Lind, *Microporous Mesoporous Mater.*, 2015, **201**, 50–60.
- 29 D. Dubbeldam, S. Calero, D. E. Ellis and R. Q. Snurr, *Mol. Simul.*, 2016, **42**, 81–101.
- 30 T. F. Willems, C. H. Rycroft, M. Kazi, J. C. Meza and M. Haranczyk, *Microporous Mesoporous Mater.*, 2012, **149**, 134–141.
- 25 31 S. L. Mayo, B. D. Olafson and W. A. Goddard, *J. Phys. Chem.*, 1990, **94**, 8897–8909.
- 32 C. E. Wilmer, K. C. Kim and R. Q. Snurr, *J. Phys. Chem. Lett.*, 2012, **3**, 2506–2511.
- 30 33 J. M. Castillo, D. Dubbeldam, T. J. H. Vlugt, B. Smit and S. Calero, *Mol. Simul.*, 2009, **35**, 1067–1076.
- 34 Y. Khalak, B. Baumeier and M. Karttunen, *J. Chem. Phys.*, 2018, **149**, 224507.
- 35 35 S. W. Rick, *J. Chem. Phys.*, 2004, **120**, 6085–6093.
- 36 S. Weerasinghe and P. E. Smith, *J. Phys. Chem. B*, 2003, **107**, 3891–3898.
- 37 H. Kokubo, J. Rösger, D. W. Bolen and B. M. Pettitt, *Biophys. J.*, 2007, **93**, 3392–3407.
- 38 B. Widom, *J. Chem. Phys.*, 1963, **39**, 2808–2812.
- 40 39 D. Frenkel and B. Smit, *Understanding Molecular Simulation*, Academic Press, Inc., USA, 2nd edn, 2001.
- 40 RASPA2 iRASPAs 2022.
- 41 M. De Pascale, M. G. De Angelis and C. Boi, *Membranes*, 2022, **12**, 203.
- 45 42 Y.-C. Cheng, C.-C. Fu, Y.-S. Hsiao, C.-C. Chien and R.-S. Juang, *J. Mol. Liq.*, 2018, **252**, 203–210.
- 43 H. Zhao, J. Huang, L. Miao, Y. Yang, Z. Xiao, Q. Chen, Q. Huang and K. Ai, *Chem. Eng. J.*, 2022, **438**, 135583.
- 44 W. Li, S. Chao, Y. Li, F. Bai, Y. Teng, X. Li, L. Li and C. Wang, *J. Membr. Sci.*, 2022, **642**, 119964.
- 45 X. Wu, Y. Hong, B. Xu, Y. Nishiyama, W. Jiang, J. Zhu, G. Zhang, S. Kitagawa and S. Horike, *J. Am. Chem. Soc.*, 2020, **142**, 14357–14364.
- 46 Structural Engineering of Two-Dimensional Covalent Organic Frameworks for Visible-Light-Driven Organic

- 1 Transformations|ACS Applied Materials & Interfaces, <https://pubs.acs.org/doi/10.1021/acsami.0c00013>, (accessed 26 June 2023).
- 47 S. Chandra, S. Kandambeth, B. P. Biswal, B. Lukose, S. M. Kunjir, M. Chaudhary, R. Babarao, T. Heine and R. Banerjee, *J. Am. Chem. Soc.*, 2013, **135**, 17853–17861.
- 5 48 Z. Kang, Y. Peng, Y. Qian, D. Yuan, M. A. Addicoat, T. Heine, Z. Hu, L. Tee, Z. Guo and D. Zhao, *Chem. Mater.*, 2016, **28**, 1277–1285.
- 10 49 E. Vitaku, C. N. Gannett, K. L. Carpenter, L. Shen, H. D. Abuña and W. R. Dichtel, *J. Am. Chem. Soc.*, 2020, **142**, 16–20.
- 50 D. Beaudoin, T. Maris and J. D. Wuest, *Nat. Chem.*, 2013, **5**, 830–834.
- 15 51 M. Huang, J. Chong, C. Hu and Y. Yang, *Inorg. Chem. Commun.*, 2020, **119**, 108094.
- 52 B. Zhang, M. Wei, H. Mao, X. Pei, S. A. Alshimri, J. A. Reimer and O. M. Yaghi, *J. Am. Chem. Soc.*, 2018, **140**, 12715–12719.
- 20 53 X. Han, J. Huang, C. Yuan, Y. Liu and Y. Cui, *J. Am. Chem. Soc.*, 2018, **140**, 892–895.
- 54 X. Li, Q. Gao, J. Wang, Y. Chen, Z.-H. Chen, H.-S. Xu, W. Tang, K. Leng, G.-H. Ning, J. Wu, Q.-H. Xu, S. Y. Quek, Y. Lu and K. P. Loh, *Nat. Commun.*, 2018, **9**, 2335.
- 55 J.-B. Liao, J.-S. Chang and D.-J. Lee, *Mater. Lett.*, 2023, **338**, 134061.
- 5 56 Q. Sun, B. Aguila and S. Ma, *Mater. Chem. Front.*, 2017, **1**, 1310–1316.
- 57 S. Kandambeth, A. Mallick, B. Lukose, M. V. Mane, T. Heine and R. Banerjee, *J. Am. Chem. Soc.*, 2012, **134**, 19524–19527.
- 10 58 S. Chandra, T. Kundu, K. Dey, M. Addicoat, T. Heine and R. Banerjee, *Chem. Mater.*, 2016, **28**, 1489–1494.
- 59 Y. Peng, G. Xu, Z. Hu, Y. Cheng, C. Chi, D. Yuan, H. Cheng and D. Zhao, *ACS Appl. Mater. Interfaces*, 2016, **8**, 18505–18512.
- 15 60 T. Kundu, J. Wang, Y. Cheng, Y. Du, Y. Qian, G. Liu and D. Zhao, *Dalton Trans.*, 2018, **47**, 13824–13829.
- 61 D. Ongari, P. G. Boyd, O. Kadioglu, A. K. Mace, S. Keskin and B. Smit, *J. Chem. Theory Comput.*, 2019, **15**, 382–401.
- 20 62 C. Cleeton, F. Lopes de Oliveira, R. Neumann, A. Farmahini, B. Luan, M. Steiner and L. Sarkisov, *Chemical Engineering and Industrial Chemistry*.

25

25

30

30

35

35

40

40

45

45

50

50

55

55