



ARCHIVIO ISTITUZIONALE DELLA RICERCA

Alma Mater Studiorum Università di Bologna Archivio istituzionale della ricerca

Viscous heating and instability of the adiabatic buoyant flows in a horizontal channel

This is the final peer-reviewed author's accepted manuscript (postprint) of the following publication:

Published Version:

Viscous heating and instability of the adiabatic buoyant flows in a horizontal channel / Barletta A.; Celli M.; Rees D.A.S.. - In: PHYSICS OF FLUIDS. - ISSN 1070-6631. - STAMPA. - 35:(2023), pp. 033111.1-033111.13. [10.1063/5.0144878]

This version is available at: <https://hdl.handle.net/11585/941365> since: 2023-09-12

Published:

DOI: <http://doi.org/10.1063/5.0144878>

Terms of use:

Some rights reserved. The terms and conditions for the reuse of this version of the manuscript are specified in the publishing policy. For all terms of use and more information see the publisher's website.

(Article begins on next page)

This item was downloaded from IRIS Università di Bologna (<https://cris.unibo.it/>).
When citing, please refer to the published version.

This is the final peer-reviewed accepted manuscript of:

A. Barletta, M. Celli, D. A. S. Rees; Viscous heating and instability of the adiabatic buoyant flows in a horizontal channel. *Physics of Fluids* 1 March 2023; 35 (3): 033111

The final published version is available online at:

<https://doi.org/10.1063/5.0144878>

Terms of use:

Some rights reserved. The terms and conditions for the reuse of this version of the manuscript are specified in the publishing policy. For all terms of use and more information see the publisher's website.

This item was downloaded from IRIS Università di Bologna (<https://cris.unibo.it/>)

When citing, please refer to the published version.

Viscous heating and instability of the adiabatic buoyant flows in a horizontal channel

A. Barletta and M. Celli

*Department of Industrial Engineering, Alma Mater Studiorum Università di Bologna,
Viale Risorgimento 2, 40136 Bologna, Italy*

D. A. S. Rees

*Department of Mechanical Engineering, University of Bath,
Bath BA2 7AY, U.K.*

(Electronic mail: antonio.barletta@unibo.it)

The stability of buoyant flows occurring in the mixed convection regime for a viscous fluid in a horizontal plane-parallel channel with adiabatic walls is investigated. The basic flow features a parallel velocity field under stationary state conditions. There exists a duality of flows, for every prescribed value of the mass flow rate across the channel cross-section, caused by the combined actions of viscous dissipation and of the buoyancy force. As pointed out in a previous study, only the primary branch of the dual solutions is compatible with the Oberbeck-Boussinesq approximation. Thus, the stability analysis will be focussed on the stability of such flows. The onset of the thermal instability with small-amplitude perturbations of the basic flow is investigated by assuming a very large Prandtl number, which is equivalent to a creeping flow regime. The neutral stability curves and the critical parametric conditions for the onset of instability are determined numerically.

I. INTRODUCTION

The instability of stationary and fully-developed flows in a plane channel is a classical topic discussed in a plethora of textbooks on fluid mechanics. Among the many, we mention Drazin and Reid¹ and Kundu, Cohen, and Dowling². The instability arises as hydrodynamic in nature when there is no thermal forcing on the flow via the boundary conditions, with the critical conditions for linear instability being determined through the solution of the Orr-Sommerfeld eigenvalue problem^{1,2}. A different conclusion is drawn when, even in the absence of an external temperature difference between the plane boundary walls, the frictional heating associated with the viscous flow is taken into account. In this case, the thermally-induced instability acts via a temperature coupling term in the local momentum balance equation. Such a term can be the viscous force as the fluid viscosity is temperature-dependent^{3,4}. An alternative scenario is the buoyancy effect, where the temperature coupling term in the momentum balance is the gravity force with a temperature-dependent fluid density modelled according to the Oberbeck-Boussinesq approximation^{5–15}.

The combined effects of buoyancy and viscous heating may yield situations where the stationary flows in a channel or duct caused by a given dynamic input, either a prescribed pressure gradient or a prescribed mass flow rate, are dual. The duality is usually accompanied by a merging between the solution branches which produces a maximum parametric condition in terms of either pressure gradient or mass flow rate above which no stationary flow is possible. This behaviour is widely documented in the literature^{8–10,12,16–18}. We mention that dual or, more generally, multiple solutions are a consequence of the nonlinearity of buoyant flows and their existence does

not necessarily imply the inclusion of the viscous dissipation term in the local energy balance equation^{19,20}.

The aim of this paper is the stability analysis of the primary branch of dual solutions found by Barletta, Celli, and Brandão¹⁸. In fact, these authors pointed out that the secondary branch refers to conditions hardly compatible with the Oberbeck-Boussinesq approximation scheme underlying their determination. The flow conditions employed in this analysis involve the fully-developed regime in a horizontal channel with thermally insulated walls. The interplay between the buoyancy force and the viscous heating of the channel flow leads to a mixed convection scenario where the velocity displays a departure from the Poiseuille profile, with a duality of solutions for every prescribed mass flow rate across the channel. Though widely described in Barletta, Celli, and Brandão¹⁸, the main features of the dual flows are surveyed also in this paper for self-containedness of our presentation and for a precise definition of which basic flow we assume when testing the transition to instability. The character of our stability analysis reflects a similar study published some years ago and relative to Darcy's flow in a fluid-saturated porous material²¹. As we are interested in the destabilising action of the viscous dissipation term in the energy balance, we will assume high viscosity and low diffusivity properties of the fluid, which means a very large Prandtl number. This assumption simplifies the governing equations for the perturbations of the basic solution as they are formulated for a creeping flow scheme with the inertial term in the momentum balance turning out to be negligible. A similar approach was followed also in Barletta and Nield⁵ and in Barletta, Celli, and Nield⁶. The focus on the creeping flow regime makes our analysis completely different from the hydrodynamically combined stability analysis of the Poiseuille flow as based on the

Orr-Sommerfeld eigenvalue problem. In fact, the hydrodynamic instability is relative to a condition where the inertial term of the momentum balance becomes utterly important for the emergence of the flow instability so that, in that case, the creeping flow scheme is inadequate^{1,2}.

An important governing parameter in the forthcoming analysis is the Gebhart number, Ge . This parameter is often employed in the literature where buoyant flows are studied by including the effect of viscous dissipation, though several authors prefer calling this parameter dissipation number, Di . Indeed, the definitions of Ge and Di are the same. The former symbol is a recognition of the pioneering study by Gebhart²², while the latter is still widely employed in the literature on geophysical flows. Among the many studies regarding the geophysical applications of the natural convection heat transfer with viscous heating, we mention the interesting papers by Kincaid and Silver²³ and by van den Berg and Yuen²⁴. The paper by Kincaid and Silver²³ provides a model where the excess heat generated in the upper part of Earth mantle during orogenesis is attributed to a viscous dissipation contribution, envisaging also cases where Di is as large as 6. In van den Berg and Yuen²⁴ the assumption $Di = 0.7$ is made on studying buoyant flows in the mantle by including the effect of viscous dissipation coupled also with the internal heating due to radioactivity and the adiabatic work induced by compression/decompression processes.

II. MATHEMATICAL MODEL

Let us consider a Newtonian fluid flowing in a plane-parallel channel bounded by walls at $z = 0$ and $z = H$. The horizontal x and y directions are unbounded, while the uniform gravitational acceleration is given by $\mathbf{g} = -g\hat{\mathbf{e}}_z$, where g is the modulus of \mathbf{g} and $\hat{\mathbf{e}}_z$ is the unit vector of the z axis. The boundary walls are both rigid and with a perfect thermal insulation.

A. Governing Equations

The Oberbeck-Boussinesq approximation can be employed so that the governing equations are written as,

$$\nabla \cdot \mathbf{u} = 0, \quad (1a)$$

$$\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} = -\frac{1}{\rho} \nabla p + g\beta(T - T_0)\hat{\mathbf{e}}_z + \nu \nabla^2 \mathbf{u}, \quad (1b)$$

$$\frac{\partial T}{\partial t} + (\mathbf{u} \cdot \nabla) T = \alpha \nabla^2 T + \frac{\nu}{c} \Phi, \quad (1c)$$

where ρ , β , ν , α and c are the fluid density, thermal expansion coefficient, kinematic viscosity, thermal diffusivity and specific heat evaluated at the constant reference temperature T_0 . In equations (1), \mathbf{u} is the velocity,

p is the local difference between the pressure and the hydrostatic pressure, T is the temperature and t is the time. Hereafter, p is called the pressure field for brevity. The symbol Φ denotes the dissipation function which, according to Einstein's notation for the implicit sums over repeated indices, can be expressed as

$$\Phi = \frac{1}{2} \gamma_{ij} \gamma_{ij} \quad \text{using} \quad \gamma_{ij} = \frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i}. \quad (2)$$

In equation (2), γ_{ij} is the shear rate tensor, while u_i and x_i denote the i th Cartesian components of the velocity vector $\mathbf{u} = (u, v, w)$ and of the position vector $\mathbf{x} = (x, y, z)$.

The boundary conditions imposed at $z = 0, H$ express impermeability, no-slip and adiabaticity,

$$\mathbf{u} = 0, \quad \frac{\partial T}{\partial z} = 0 \quad \text{for} \quad z = 0, H. \quad (3)$$

B. Dimensionless Formulation

Dimensionless quantities can be defined through the scaling

$$\begin{aligned} \frac{\mathbf{x}}{H} &\rightarrow \mathbf{x}, & \frac{t}{H^2/\alpha} &\rightarrow t, & \frac{\mathbf{u}}{\alpha/H} &\rightarrow \mathbf{u}, \\ \frac{p}{\rho\alpha\nu/H^2} &\rightarrow p, & \frac{T - T_0}{\Delta T} &\rightarrow T, \\ \frac{\Phi}{\alpha^2/H^4} &\rightarrow \Phi, & \text{using} \quad \Delta T &= \frac{\alpha\nu}{g\beta H^3}. \end{aligned} \quad (4)$$

On account of equation (4), equations (1) and (3) can be rewritten in a dimensionless form as

$$\nabla \cdot \mathbf{u} = 0, \quad (5a)$$

$$\frac{1}{Pr} \left[\frac{\partial \mathbf{u}}{\partial t} + (\mathbf{u} \cdot \nabla) \mathbf{u} \right] = -\nabla p + T \hat{\mathbf{e}}_z + \nabla^2 \mathbf{u}, \quad (5b)$$

$$\frac{\partial T}{\partial t} + (\mathbf{u} \cdot \nabla) T = \nabla^2 T + Ge \Phi, \quad (5c)$$

with

$$\mathbf{u} = 0, \quad \frac{\partial T}{\partial z} = 0 \quad \text{for} \quad z = 0, 1. \quad (6)$$

In equations (5b) and (5c), the Prandtl number, Pr , and the Gebhart number, Ge , are defined as

$$Pr = \frac{\nu}{\alpha}, \quad Ge = \frac{g\beta H}{c}. \quad (7)$$

III. BASIC DUAL FLOWS

In this section, we survey the main features of the dual adiabatic flows relying on the results conveyed in a previous study¹⁸. Stationary solutions of equations (5) and

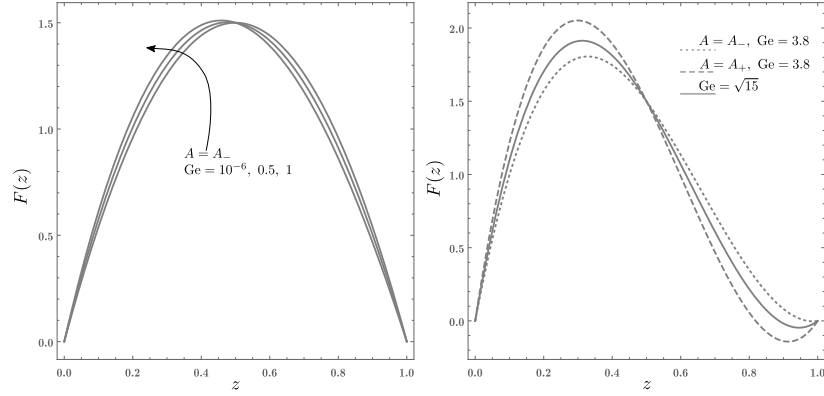


FIG. 1. Plots of $F(z)$ for either $A = A_-$ or $A = A_+$ with different values of Ge

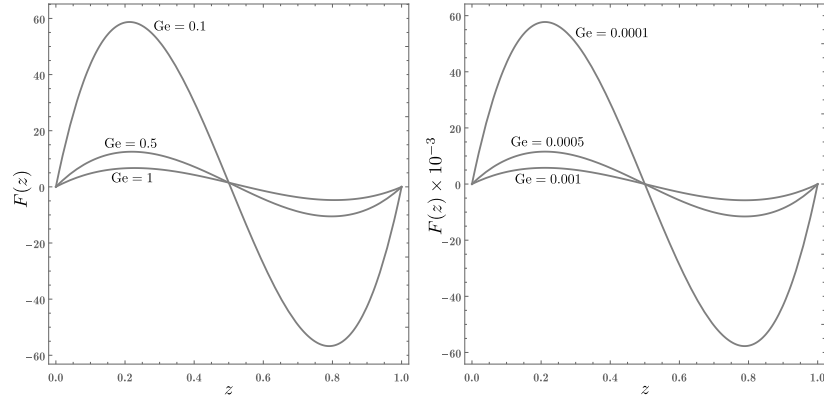


FIG. 2. Plots of $F(z)$ for $A = A_+$ with different values of Ge

(6) with a parallel velocity field can be expressed as

$$\begin{aligned} u_b &= Pe F(z) \cos \varphi, & v_b &= Pe F(z) \sin \varphi, & w_b &= 0, \\ T_b &= Pe F'''(z) (x \cos \varphi + y \sin \varphi) + Pe^2 G(z), \\ \nabla p_b &= (Pe F''(z) \cos \varphi, Pe F''(z) \sin \varphi, T_b), \end{aligned} \quad (8)$$

where the subscript b indicates “basic solution”, Pe is the Péclet number and the primes denote the derivatives with respect to z , while functions $F(z)$ and $G(z)$ are polynomials given by

$$\begin{aligned} F(z) &= z(1-z)[A - 2(A-6)z], \\ G(z) &= \frac{z^2}{10} \{ -5A^2 Ge + 20A[(A-4)Ge + A-6]z \\ &\quad - 10[A^2(4Ge+3) - 30A(Ge+1) + 48Ge + 72]z^2 \\ &\quad + 12(A-6)[3(A-4)Ge + A-6]z^3 \} \end{aligned}$$

$$-12(A-6)^2 Ge z^4 \}. \quad (9)$$

The constant A can be equal either to A_- or A_+ , where

$$\begin{aligned} A_- &= 2 \frac{3Ge + 15 - \sqrt{15(15 - Ge^2)}}{Ge}, \\ A_+ &= 2 \frac{3Ge + 15 + \sqrt{15(15 - Ge^2)}}{Ge}. \end{aligned} \quad (10)$$

Equations (8)-(10) describe horizontal parallel flows in the xy plane where the velocity field is inclined an angle φ to the x axis. The twofold expression of $A = A_{\pm}$ means that there are dual flows corresponding to the same prescribed Péclet and Gebhart numbers. Such dual flows exist if $Ge \leq \sqrt{15} \approx 3.87298$ and they coincide only when $Ge = \sqrt{15}$. We note that such an upper bound for Ge is

an extremely large value in practical cases¹⁸. The Péclet number is defined in terms of dimensional quantities as

$$\text{Pe} = \frac{U_0 H}{\alpha}, \quad (11)$$

where the reference dimensional velocity U_0 is intended as the basic average velocity in the horizontal flow direction defined by the unit vector $(\cos \varphi, \sin \varphi, 0)$. In fact, equation (9) yields

$$\int_0^1 F(z) dz = 1, \quad (12)$$

which means that the average dimensionless velocity in the flow direction is equal to Pe .

It is to be mentioned that function $G(z)$ is defined only up to an arbitrary additive constant which, in equation (9), has been fixed so that $G(0) = 0$. Such a feature is due to the Neumann boundary conditions for the temperature which leave this constant undetermined. The temperature appears on the right hand side of equation (5b) next to the ∇p term. Thus, changing the temperature by an additive constant has the physical meaning of changing the reference temperature value employed for the formulation of the Oberbeck-Boussinesq approximation. This change leads to a redetermination of the hydrostatic pressure and to a resulting modification in the dimensional field p which, by definition, is the difference between the pressure and the hydrostatic pressure. In fact, the hydrostatic pressure is $-\rho g z$, where ρ is the fluid density evaluated at the reference temperature T_0 . It becomes clear that altering the arbitrary additive constant in $G(z)$ influences the basic solution only by modifying, through an overall additive constant, the local values of T_b and, as a consequence of equation (9), also of $\partial p_b / \partial z$. On the other hand, the discussion of the stability of the dual basic flows, to be carried out later on, is not affected in any way by the choice of the arbitrary additive constant in the expression of $G(z)$. In fact, it will be shown that the dynamics of perturbations is governed by partial differential equations where ∇p_b is absent and T_b is present only through its gradient.

The physical effects underlying the basic dual solutions are the imposed horizontal flow rate causing the viscous heating and the buoyancy force induced by the resulting temperature gradient. Such effects become inactive when $\text{Ge} \rightarrow 0$, as highlighted by equation (5c), and the basic solution becomes an isothermal Poiseuille flow. This conclusion is made evident by taking the power series expansions of A_+ and A_- at small Ge ,

$$\begin{aligned} A_- &= 6 + \text{Ge} + \mathcal{O}(\text{Ge}^2), \\ A_+ &= \frac{60}{\text{Ge}} + 6 - \text{Ge} + \mathcal{O}(\text{Ge}^2). \end{aligned} \quad (13)$$

Equation (13) yields $A_- = 6$, when $\text{Ge} \rightarrow 0$, while A_+ becomes singular. Hence, the A_+ -branch of the dual flows

blows up when $\text{Ge} \rightarrow 0$, while the A_- -branch yields

$$\begin{aligned} u_b &= 6 \text{Pe} z (1 - z) \cos \varphi, \\ v_b &= 6 \text{Pe} z (1 - z) \sin \varphi, \quad w_b = 0, \quad T_b = 0, \\ \nabla p_b &= (-12 \text{Pe} \cos \varphi, -12 \text{Pe} \sin \varphi, 0). \end{aligned} \quad (14)$$

Equation (14) represents the isothermal Poiseuille flow in the direction defined by the unit vector $(\cos \varphi, \sin \varphi, 0)$.

We note that, in every case where $\text{Ge} \neq 0$, the basic temperature gradient is inclined to the horizontal with constant horizontal components in the x and y directions. This feature is easily spotted by reckoning from equation (9) that $F'''(z) = 12(A - 6)$.

Figures 1 and 2 illustrate the velocity profiles as plots of $F(z)$ for various Gebhart numbers and for both branches $A = A_-$ and $A = A_+$. The $A = A_-$ branch shows very small departures from the Poiseuille profile unless the Gebhart number becomes huge, namely, close to its upper bound $\text{Ge} = \sqrt{15}$. This feature is clearly visible in Fig. 1, while Fig. 2 reveals that the $A = A_+$ branch marks a sharp departure from the Poiseuille profile especially at small Gebhart numbers. The characteristics of the $A = A_+$ profiles show a bidirectional nature of the flow which arises also, albeit in a minimal way, for the $A = A_-$ profiles, but only when Ge is very close to its upper bound $\sqrt{15}$. Figure 2 also shows that, at small Gebhart numbers, $F(z)$ for the $A = A_+$ branch scales proportionally to Ge^{-1} , approximately. This feature is easily recognised on comparing the left-hand frame and the right-hand frame of Fig. 2, and it is proved on expanding $F(z)$ in a power series of Ge for $A = A_+$,

$$F(z) = \frac{60 z (1 - z) (1 - 2z)}{\text{Ge}} + 6(1 - z)z + \mathcal{O}(\text{Ge}). \quad (15)$$

The vertical change of the basic temperature field is illustrated in Figs. 3 and 4 by plotting function $G(z)$ with different values of Ge for the $A = A_-$ and $A = A_+$ branches. Figure 3 shows that the $A = A_-$ branch features a significant dependence of the temperature profiles on Ge , despite the weak influence of the Gebhart number on the velocity profiles as already pointed out while commenting on Fig. 1. Figure 4 shows that, at small Ge and for the $A = A_+$ branch, function $G(z)$ scales proportionally to Ge^{-2} , approximately. This behaviour is shown through a power series expansion of $G(z)$ with $A = A_+$,

$$\begin{aligned} G(z) &= \frac{720 z^3 (6 z^2 - 15 z + 10)}{\text{Ge}^2} \\ &\quad - \frac{360 z^2 (1 - z)^2 (12 z^2 - 12 z + 5)}{\text{Ge}} \\ &\quad + 72 z^2 (4 z^3 - 10 z^2 + 10 z - 5) + \mathcal{O}(\text{Ge}). \end{aligned} \quad (16)$$

A remarkable feature revealed by Fig. 3 is the unstable thermal stratification ($\partial T_b / \partial z < 0$) for the $A = A_-$ branch occurring at the lower part of the channel. Such

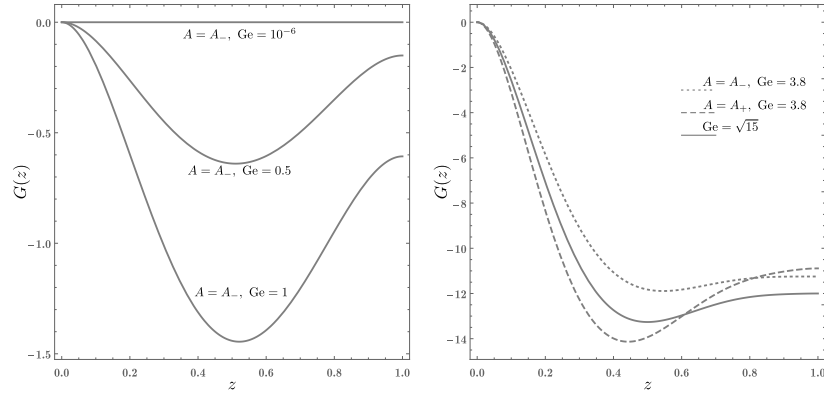


FIG. 3. Plots of $G(z)$ for either $A = A_-$ or $A = A_+$ with different values of Ge

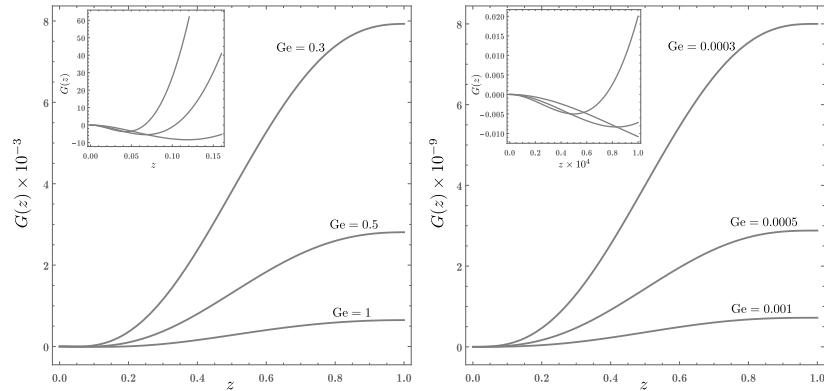


FIG. 4. Plots of $G(z)$ for $A = A_+$ with different values of Ge

an unstable thermal stratification does emerge for all Gebhart numbers also with the $A = A_+$ branch, although it can be visualised in Fig. 4 only through the miniatures at small values of z . Analytically, this conclusion can be inferred by evaluating $G''(0)$ with $A = A_+$,

$$G''(0) = -24 Ge^{-1} \left[(Ge + 5) \sqrt{15(15 - Ge^2)} + Ge(15 - Ge) + 75 \right]. \quad (17)$$

The right hand side of equation (17) is evidently negative for every $Ge \leq \sqrt{15}$. As a consequence, there always exist regions close to $z = 0$ where $G'(z) < 0$.

The existence of a region inside the channel with a negative z component of the basic temperature gradient for either the $A = A_-$ branch or the $A = A_+$ branch discloses the possibility of a thermal instability of the Rayleigh-Bénard type (heating from below) for the dual

basic flows. This circumstance will be explored later on. It is to be mentioned that the vertical component of the basic temperature gradient is not the only source of a possible thermal instability. In fact, the constant horizontal components of ∇T_b may contribute possibly leading to a thermal instability of the Hadley-type.

It has been pointed out that the $A = A_+$ branch can hardly be considered compatible with the Oberbeck-Boussinesq approximate model underlying the existence of the dual solutions¹⁸. The reason is that the approximate model requires the product between the thermal expansion coefficient β and the maximum temperature difference across the flow domain to be much smaller than unity. As pointed out by Barletta, Celli, and Brandão¹⁸, this condition is precluded when considering the $A = A_+$ branch of the dual solutions. On account of these findings, the forthcoming stability analysis will be focussed

just on the $A = A_-$ branch.

IV. DYNAMICS OF SMALL-AMPLITUDE PERTURBATIONS

Let us perturb the basic dual flows,

$$\begin{pmatrix} \mathbf{u} \\ p \\ T \end{pmatrix} = \begin{pmatrix} \mathbf{u}_b \\ p_b \\ T_b \end{pmatrix} + \varepsilon \begin{pmatrix} \mathbf{U} \\ P \\ \Theta \end{pmatrix}, \quad (18)$$

where ε is the perturbation parameter and (\mathbf{U}, P, Θ) are the perturbations of velocity, pressure and temperature, respectively. The Cartesian components of \mathbf{U} are denoted as (U, V, W) . Let us substitute equation (18) into equations (5) and (6) by employing equations (2) and (8), namely

$$\nabla \cdot \mathbf{U} = 0, \quad (19a)$$

$$\frac{1}{\text{Pr}} \left[\frac{\partial \mathbf{U}}{\partial t} + (\mathbf{u}_b \cdot \nabla) \mathbf{U} + (\mathbf{U} \cdot \nabla) \mathbf{u}_b \right] = -\nabla P + \Theta \hat{\mathbf{e}}_z + \nabla^2 \mathbf{U}, \quad (19b)$$

$$\begin{aligned} & \frac{\partial \Theta}{\partial t} + (\mathbf{u}_b \cdot \nabla) \Theta + (\mathbf{U} \cdot \nabla) T_b \\ &= \nabla^2 \Theta + 2 \text{Ge} \left[\left(\frac{\partial U}{\partial z} + \frac{\partial W}{\partial x} \right) u'_b \right. \\ & \quad \left. + \left(\frac{\partial V}{\partial z} + \frac{\partial W}{\partial y} \right) v'_b \right], \end{aligned} \quad (19c)$$

$$\mathbf{U} = 0, \quad \frac{\partial \Theta}{\partial z} = 0 \quad \text{for } z = 0, 1, \quad (19d)$$

where terms $\mathcal{O}(\varepsilon^2)$ have been neglected in order to account for small-amplitude perturbations.

Since the basic flow direction is inclined an angle φ to the x direction, the x axis defines an arbitrary horizontal direction, so that the normal modes of perturbation can be expressed as plane waves propagating along the x -direction. The effect of arbitrary oblique modes can be tested by allowing a changing angle within the range $0 \leq \varphi \leq \pi/2$. The values $\varphi = 0$ and $\varphi = \pi/2$ yield the transverse modes and the longitudinal modes, respectively. Thus, we write

$$\begin{pmatrix} \mathbf{U} \\ P \\ \Theta \end{pmatrix} = \begin{pmatrix} \hat{\mathbf{U}}(z) \\ \hat{P}(z) \\ \hat{\Theta}(z) \end{pmatrix} e^{ikx} e^{\lambda t}, \quad (20)$$

where k is the real-valued wavenumber, while λ is a complex-valued parameter. The real and imaginary parts of λ are denoted as $\lambda = \eta - i\omega$, with η expressing the growth rate and ω yielding the angular frequency. Linear instability is identified with the condition $\eta > 0$, while $\eta = 0$ expresses the threshold case of neutral stability. We substitute equation (20) into equations (19), so that

we can write

$$ik\hat{U} + \hat{W}' = 0, \quad (21a)$$

$$\begin{aligned} & \frac{1}{\text{Pr}} \left(\lambda \hat{U} + ik u_b \hat{U} + \hat{W} u'_b \right) \\ &= -ik\hat{P} + \hat{U}'' - k^2 \hat{U}, \end{aligned} \quad (21b)$$

$$\frac{1}{\text{Pr}} \left(\lambda \hat{V} + ik u_b \hat{V} + \hat{W} v'_b \right) = \hat{V}'' - k^2 \hat{V}, \quad (21c)$$

$$\frac{1}{\text{Pr}} \left(\lambda \hat{W} + ik u_b \hat{W} \right) = -\hat{P}' + \hat{\Theta} + \hat{W}'' - k^2 \hat{W}, \quad (21d)$$

$$\begin{aligned} & \lambda \hat{\Theta} + ik u_b \hat{\Theta} + \hat{U} \frac{\partial T_b}{\partial x} + \hat{V} \frac{\partial T_b}{\partial y} + \hat{W} \frac{\partial T_b}{\partial z} \\ &= \hat{\Theta}'' - k^2 \hat{\Theta} + 2 \text{Ge} \left[\left(\hat{U}' + ik \hat{W} \right) u'_b + \hat{V}' v'_b \right], \end{aligned} \quad (21e)$$

$$\begin{aligned} & \hat{U} = 0, \quad \hat{V} = 0, \quad \hat{W} = 0 \\ & \hat{\Theta}' = 0 \quad \text{for } z = 0, 1, \end{aligned} \quad (21f)$$

where $(\hat{U}, \hat{V}, \hat{W})$ are the Cartesian components of $\hat{\mathbf{U}}$.

The physically significant situation where the viscous dissipation effect is expected to cause the instability is when the fluid has a large kinematic viscosity combined with a small thermal diffusivity. Roughly speaking, such fluids are markedly susceptible to frictional heating while the diffusion of such an internally generated heat is inefficient. This situation reasonably occurs when the Prandtl number is extremely large.

A. Creeping Flow

A regime of creeping flow occurs when the inertial terms in the momentum balance are negligible. This happens when the limit $\text{Pr} \rightarrow \infty$ is taken for equation (19b). As mentioned above, such a limit identifies a condition where an extremely viscous fluid is employed having a small thermal diffusivity. In this limit, equations (21) simplify to

$$ik\hat{U} + \hat{W}' = 0, \quad (22a)$$

$$-ik\hat{P} + \hat{U}'' - k^2 \hat{U} = 0, \quad (22b)$$

$$\hat{V}'' - k^2 \hat{V} = 0, \quad (22c)$$

$$-\hat{P}' + \hat{\Theta} + \hat{W}'' - k^2 \hat{W} = 0, \quad (22d)$$

$$\begin{aligned} & \lambda \hat{\Theta} + ik u_b \hat{\Theta} + \hat{U} \frac{\partial T_b}{\partial x} + \hat{V} \frac{\partial T_b}{\partial y} + \hat{W} \frac{\partial T_b}{\partial z} \\ &= \hat{\Theta}'' - k^2 \hat{\Theta} + 2 \text{Ge} \left[\left(\hat{U}' + ik \hat{W} \right) u'_b + \hat{V}' v'_b \right], \end{aligned} \quad (22e)$$

$$\begin{aligned} & \hat{U} = 0, \quad \hat{V} = 0, \quad \hat{W} = 0 \\ & \hat{\Theta}' = 0 \quad \text{for } z = 0, 1. \end{aligned} \quad (22f)$$

From equations (22c) and (22f), one can immediately conclude that $\hat{V} = 0$ in the whole range $0 \leq z \leq 1$. Furthermore, by employing equations (22a) and (22b), one can express \hat{U} and \hat{P} in terms of \hat{W} and its derivatives.

Thus, one is led to a reformulation of equations (22) involving only the unknowns \hat{W} and $\hat{\Theta}$,

$$\hat{W}'''' - 2k^2 \hat{W}'' + k^4 \hat{W} - k^2 \hat{\Theta} = 0, \quad (23a)$$

$$\begin{aligned} \hat{\Theta}'' - [k^2 + \lambda + i k \text{Pe} F(z) \cos \varphi] \hat{\Theta} \\ + \frac{2 i \text{Ge} \text{Pe} F'(z) \cos \varphi}{k} (\hat{W}'' + k^2 \hat{W}) \\ - \frac{i \text{Pe} F'''(z) \cos \varphi}{k} \hat{W}' - \text{Pe}^2 G'(z) \hat{W} = 0, \end{aligned} \quad (23b)$$

$$\hat{W} = 0, \quad \hat{W}' = 0, \quad \hat{\Theta}' = 0 \quad \text{for } z = 0, 1. \quad (23c)$$

Creeping flow is usually associated with a regime of extremely small Reynolds number, $\text{Re} = \text{Pe}/\text{Pr}$. From the mathematical viewpoint, creeping flow means a situation where the limit $\text{Re} \rightarrow 0$ is combined with the limit $\text{Pr} \rightarrow \infty$. These limits can be taken on keeping $\text{Pe} = \text{Re} \text{Pr} \sim O(1)$. In the following, we will consider the dynamics of perturbations as modelled by a creeping flow achieved with a finite Péclet number.

The linear analysis of the instability for the basic flows defined by equations (8)–(10) is carried out by solving numerically the eigenvalue problem (23). The solution is sought by fixing the input parameters (φ, Ge) and by determining the neutral stability threshold value of Pe versus the wavenumber k . The angular frequency, ω , of the neutrally stable modes is also determined.

The neutral stability threshold implies a zero growth rate, η . Additionally, for the sake of convenience, the basic average velocity is taken into account by redefining the angular frequency in the comoving reference frame, namely

$$\hat{\omega} = \omega - k \text{Pe} \cos \varphi. \quad (24)$$

Thus, equations (23) can be rewritten as

$$\hat{W}'''' - 2k^2 \hat{W}'' + k^4 \hat{W} - k^2 \hat{\Theta} = 0, \quad (25a)$$

$$\begin{aligned} \hat{\Theta}'' - [k^2 - i \hat{\omega} + i k \text{Pe} \hat{F}(z) \cos \varphi] \hat{\Theta} \\ + \frac{2 i \text{Ge} \text{Pe} \hat{F}'(z) \cos \varphi}{k} (\hat{W}'' + k^2 \hat{W}) \\ - \frac{i \text{Pe} \hat{F}'''(z) \cos \varphi}{k} \hat{W}' - \text{Pe}^2 G'(z) \hat{W} = 0, \end{aligned} \quad (25b)$$

$$\hat{W} = 0, \quad \hat{W}' = 0, \quad \hat{\Theta}' = 0 \quad \text{for } z = 0, 1, \quad (25c)$$

where $\hat{F}(z) = F(z) - 1$ is a function with a zero average value over the interval $0 \leq z \leq 1$, as a consequence of equation (12). By assigning φ as an input datum for the solution of equations (25), one actually defines the type of oblique modes perturbing the flow, with the transverse modes ($\varphi = 0$) and the longitudinal modes ($\varphi = \pi/2$) as limiting cases.

V. DISCUSSION OF THE RESULTS

We pointed out in Section III that the linear stability analysis is relative to the $A = A_-$ branch of the

dual flows. The numerical solution of the stability eigenvalue problem (25) is sought by employing the shooting method. We do not go into the details of this numerical technique as its use for the solution of flow stability eigenvalue problems has been widely discussed elsewhere^{25,26}.

The software tool actually employed to implement the shooting method is *Mathematica* (© Wolfram Research, Inc.) with its functions *NDSolve* and *FindRoot*. The former function serves to solve the initial value problem based on equations (25), starting at $z = 0$, while the latter function solves the target conditions (25c) at $z = 1$, thus yielding the numerical values for the neutral stability output data ($\hat{\omega}, \text{Pe}$). The neutral stability condition is represented by the curve in the parametric (k, Pe) plane, with the minimum Pe point along the curve yielding the critical condition for the onset of instability. Such a critical condition is given by $k = k_c$ and $\text{Pe} = \text{Pe}_c$, where the subscript c stands for critical value. Tracing the dependence of Pe_c on the inclination angle φ of the perturbation mode in different cases allows one to establish which modes are the most effective at onset of instability. Then, the stability analysis can be focussed just on those modes.

A. The Most Unstable Perturbations

We start the stability analysis from high values of Ge , namely $\text{Ge} = \sqrt{15}$ and $\text{Ge} = 2$. The neutral stability curves in the (k, Pe) plane are drawn in Fig. 5 for the transverse and the longitudinal modes. We point out that $\text{Ge} = \sqrt{15}$ is the highest possible value of the Gebhart number. In fact, such a value is the highest possible according to the mathematical definition of the dual solutions, but we stress that this value is extremely large for physical systems. Figure 5 reveals that, both for $\text{Ge} = \sqrt{15}$ and $\text{Ge} = 2$, the longitudinal modes are the more unstable as they yield the transition to instability with lower values of Pe for every k . The neutral stability curves for longitudinal modes reveal also that a finite value of Pe is achieved when $k \rightarrow 0$. This feature has been observed also in the study of the Rayleigh-Bénard instability when Neumann boundary conditions for the temperature are utilised, instead of the usual Dirichlet temperature conditions²⁷. We point out that the critical value of Pe for longitudinal modes is obtained for $k \rightarrow 0$ in the case $\text{Ge} = \sqrt{15}$, but for a nonzero k with $\text{Ge} = 2$ though hardly evident in Fig. 5. More precisely, one finds

$$k_c = 0.842235, \quad \text{Pe}_c = 17.4116, \quad \text{for } \text{Ge} = 2. \quad (26)$$

We also note that the neutral stability curve for transverse modes is disconnected in two parts when $\text{Ge} = \sqrt{15}$. These disconnected parts join in a single curve when $\text{Ge} = 2$, thus forming a local maximum of Pe versus k .

The conclusion that longitudinal modes are the most unstable is confirmed by Fig. 6 which is relative to $\text{Ge} = 1$ and $\text{Ge} = 0.5$. For both values of Ge , the critical condition $\text{Pe} = \text{Pe}_c$ occurs for longitudinal modes with a

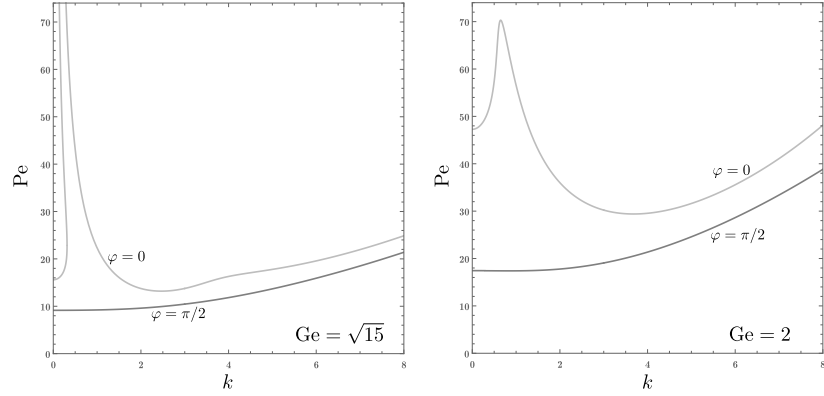


FIG. 5. Neutral stability curves in the (k, Pe) plane for transverse (light grey line, $\varphi = 0$) and longitudinal (dark grey line, $\varphi = \pi/2$) modes

nonzero k_c . There is a markedly different shape of the neutral stability curves for transverse modes with $Ge = 1$ and $Ge = 0.5$ compared to that for $Ge = 2$ (Fig. 5). Such a diversion is due to the very steep increase of the neutral stability value of Pe in the limit $k \rightarrow 0$ when Ge decreases below 2.

A more systematic study of the effects of the inclination angle, φ , on the instability threshold is carried out by testing the dependence of the critical Péclet number on this angle. Together with the huge values of Ge considered in Figs. 5 and 6, smaller and gradually more realistic values of Ge are considered in Fig. 7. This figure shows the change of Pe_c with φ for oblique modes. The change is monotonic with the case $\varphi = \pi/2$ (longitudinal modes) displaying the minimum value of Pe_c , in all case examined. This means that the statement that longitudinal modes are those selected at onset of instability can be assumed of a general validity. Figure 7 reveals that the sensitivity of Pe_c to φ becomes stronger as Ge decreases. Another important fact is that the critical value of Pe is achieved with either $k_c = 0$ or $k_c \neq 0$ for different ranges of φ . Indeed, such a complicated trend is a peculiarity for those cases where Ge is very large, $\sqrt{15}$ or 2 among the values examined in Fig. 7. For smaller Gebhart numbers, the critical conditions are always associated with $k_c \neq 0$ for every φ .

B. The Longitudinal Modes

Since we established that the longitudinal modes identify the onset of the instability, we will now restrict our attention to these modes. Then, the stability eigenvalue problem (25) is greatly simplified,

$$\hat{W}'''' - 2k^2 \hat{W}'' + k^4 \hat{W} - k^2 \hat{\Theta} = 0, \quad (27a)$$

$$\hat{\Theta}'' - (k^2 - i\hat{\omega}) \hat{\Theta} - Pe^2 G'(z) \hat{W} = 0, \quad (27b)$$

$$\hat{W} = 0, \quad \hat{W}' = 0, \quad \hat{\Theta} = 0 \quad \text{for } z = 0, 1. \quad (27c)$$

The most important feature of equations (27) is that neutral stability with longitudinal modes occurs with $\hat{\omega} = \omega = 0$, where the equality $\hat{\omega} = \omega$ is a consequence of the definition (24). This feature, which can be designated as a principle of exchange of stabilities, cannot be proved rigorously though it can be inferred quite clearly from the numerical data.

1. The Limit of Small Gebhart Numbers

A physically significant asymptotic condition is associated with the double limit $Ge \rightarrow 0$ and $Pe \rightarrow \infty$ on keeping $Ge Pe^2 \sim \mathcal{O}(1)$. Beyond its mathematical formulation, this asymptotic behaviour means that with small values of Ge the neutral stability threshold for Pe scales proportionally to $Ge^{-1/2}$.

By expanding $G'(z)$ in a power series of Ge , on account of equations (9) and (10) and of the choice $A = A_-$, we obtain

$$G'(z) = -36 Ge (2z^3 - 3z^2 + z) + \mathcal{O}(Ge^2). \quad (28)$$

We also introduce the parameter

$$\mathcal{R} = Pe \sqrt{Ge}. \quad (29)$$

Thus, with $Ge \rightarrow 0$ and $\mathcal{R} \sim \mathcal{O}(1)$, equations (27) and (28) yield

$$\hat{W}'''' - 2k^2 \hat{W}'' + k^4 \hat{W} - k^2 \hat{\Theta} = 0, \quad (30a)$$

$$\hat{\Theta}'' - (k^2 - i\hat{\omega}) \hat{\Theta} + 36 \mathcal{R}^2 (2z^3 - 3z^2 + z) \hat{W} = 0, \quad (30b)$$

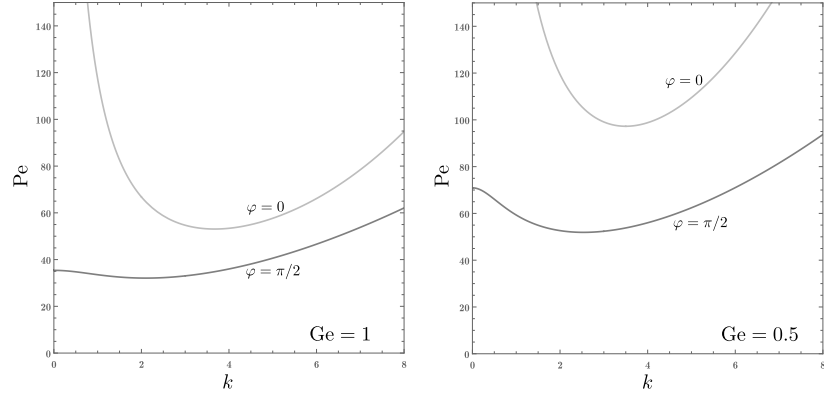


FIG. 6. Neutral stability curves in the (k, Pe) plane for transverse (light grey line, $\varphi = 0$) and longitudinal (dark grey line, $\varphi = \pi/2$) modes

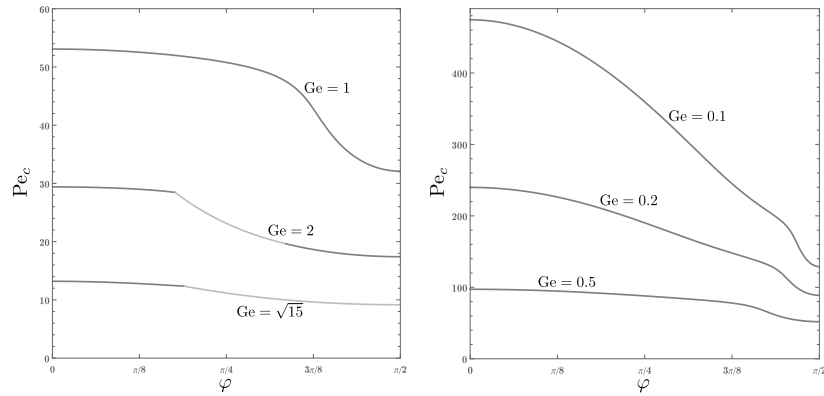


FIG. 7. Critical values of Pe versus φ for oblique modes. Light grey lines denote $k_c = 0$ critical conditions, while dark grey lines denote $k_c \neq 0$ critical conditions

$$\hat{W} = 0, \quad \hat{W}' = 0, \quad \hat{\Theta}' = 0 \quad \text{for } z = 0, 1. \quad (30c)$$

We note that, in equations (30), Ge and Pe do not appear separately but only through the parameter \mathcal{R} . Hence, the neutral stability in the limit $Ge \rightarrow 0$ can be formulated as a threshold condition for the parameter \mathcal{R} . We also point out that \mathcal{R}^2 can be interpreted as a viscous dissipation based Rayleigh number

$$\mathcal{R}^2 = \frac{g \beta \Delta T_{vd} H^3}{\nu \alpha}, \quad \text{where } \Delta T_{vd} = \frac{\mu U_0^2}{\chi}, \quad (31)$$

and equations (7) and (11) have been used. Here, μ is the dynamic viscosity of the fluid and χ its thermal conductivity, while ΔT_{vd} is a dimensional temperature difference characteristic of the viscous dissipation effect.

The numerical solution of equations (30) allows one to obtain the neutral stability curve in the (k, \mathcal{R}) plane for the limiting case of small- Ge , as illustrated in Fig. 8. An important feature is that, unlike the neutral stability curves for finite nonzero values of Ge shown in Figs. 5 and 6, the ordinate axis $k = 0$ is a vertical asymptote for the neutral stability curve shown in Fig. 8. In fact, the critical data for the small- Ge asymptotic solution are

$$k_c = 2.88872, \quad \mathcal{R}_c = 41.8534 \quad (32)$$

Equation (32) is the basis for determining the trend of Pe_c versus Ge at small values of Ge . In particular, equations (29) and (32) imply that $Pe_c \sim \mathcal{O}(Ge^{-1/2})$. This result is interesting as it differs significantly from the behaviour observed in the case of the adiabatic Darcy's

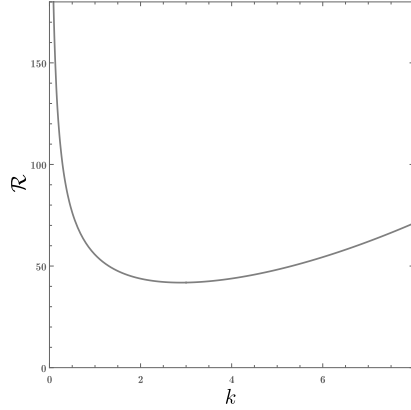


FIG. 8. Longitudinal modes: neutral stability curve in the (k, \mathcal{R}) plane for the asymptotic condition $\text{Ge} \rightarrow 0$

flow in a porous medium²¹. In that case, it has been proved by Barletta and Rees²¹ that the small- Ge trend of Pe_c is such that $\text{Pe}_c \sim \mathcal{O}(\text{Ge}^{-1})$. In other words, for Darcy's flow in a porous medium, Pe_c diverges to infinity for $\text{Ge} \rightarrow 0$ significantly faster than in the case of Newtonian flow. The reason of the difference between these cases relies in the derivative $\partial T_b / \partial z$, which drives the instability for longitudinal modes. As $\text{Ge} \rightarrow 0$, one can infer from equations (8), (9) and (10) with $A = A_-$ that $\partial T_b / \partial z \sim \mathcal{O}(\text{Ge} \text{Pe}^2)$. The corresponding result in the case of Darcy's flow is $\partial T_b / \partial z \sim \mathcal{O}(\text{Ge}^2 \text{Pe}^2)$ as demonstrated in Barletta and Rees²¹.

2. The Neutral Stability Condition for $k \rightarrow 0$

It has been pointed out that, for every $\text{Ge} \neq 0$, the neutral stability condition for longitudinal modes suggests a finite value of Pe for infinite wavelenght modes, *i.e.*, for the limit $k \rightarrow 0$. This conjectured trend can be verified analytically by employing a power series solution of the eigenvalue problem (27). We set $\hat{\omega} = 0$ and adopt the expansions in even powers of k given by

$$\begin{aligned}\hat{W}(z) &= \hat{W}_0(z) + \hat{W}_2(z)k^2 + \hat{W}_4(z)k^4 + \mathcal{O}(k^6), \\ \hat{\Theta}(z) &= \hat{\Theta}_0(z) + \hat{\Theta}_2(z)k^2 + \hat{\Theta}_4(z)k^4 + \mathcal{O}(k^6), \\ \text{Pe} &= \text{Pe}_0 + \text{Pe}_2k^2 + \text{Pe}_4k^4 + \mathcal{O}(k^6).\end{aligned}\quad (33)$$

By substituting equation (33) into equations (27) we obtain, to zero order in k ,

$$\hat{W}_0'''' = 0, \quad (34a)$$

$$\hat{\Theta}_0'' - \text{Pe}_0^2 G'(z) \hat{W}_0 = 0, \quad (34b)$$

$$\begin{aligned}\hat{W}_0(0) &= 0, \quad \hat{W}_0'(0) = 0, \quad \hat{\Theta}_0(0) = 0, \\ \hat{W}_0(1) &= 0, \quad \hat{W}_0'(1) = 0, \quad \hat{\Theta}_0(1) = 0.\end{aligned}\quad (34c)$$

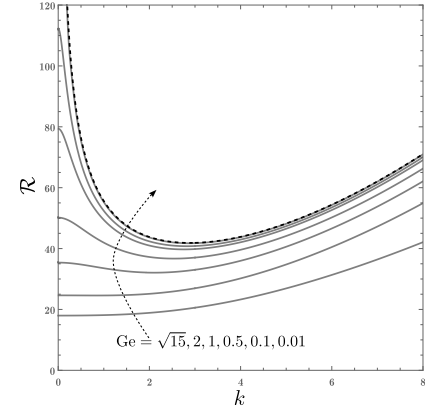


FIG. 9. Longitudinal modes: neutral stability curves in the (k, \mathcal{R}) plane for different values of Ge . The dashed neutral stability curve indicates the asymptotic condition $\text{Ge} \rightarrow 0$

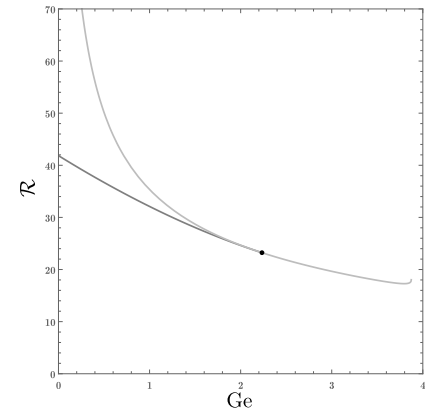


FIG. 10. Longitudinal modes: \mathcal{R}_c versus Ge (dark grey line) compared with \mathcal{R}_0 versus Ge (light grey line). The black dot denotes the transition from $k_c \neq 0$ to $k_c = 0$ occurring when Ge is given by equation (40)

The solution of equations (34) is

$$\hat{W}_0(z) = 0, \quad \hat{\Theta}_0(z) = 1, \quad (35)$$

while Pe_0 remains yet undetermined.

Indeed, $\hat{\Theta}_0(z)$ could be equal to any constant value as the original problem (27) is homogeneous. Choosing the constant value 1 in equation (35) means getting rid of the scale invariance for the eigenfunctions by implicitly fixing the extra condition $\hat{\Theta}(0) = 1$. The immediate consequence is that $\hat{\Theta}_n(0) = 0$ for every positive integer n . Therefore, the system obtained from equations (27) to

second order in k is given by

$$\hat{W}_2'''' - 1 = 0, \quad (36a)$$

$$\hat{\Theta}_2'' - 1 - \text{Pe}_0^2 G'(z) \hat{W}_2 = 0, \quad (36b)$$

$$\begin{aligned} \hat{W}_2(0) = 0, \quad \hat{W}_2'(0) = 0, \quad \hat{\Theta}_2(0) = 0, \quad \hat{\Theta}_2'(0) = 0, \\ \hat{W}_2(1) = 0, \quad \hat{W}_2'(1) = 0. \end{aligned} \quad (36c)$$

There should also be an extra condition $\hat{\Theta}_2'(1) = 0$, but it is not needed to determine the solution of equations (36). We do not report such a solution for the sake of brevity. We just say that $\hat{W}_2(z)$ is a fourth-degree polynomial in z , while $\hat{\Theta}_2(z)$ is an eleventh-degree polynomial in z .

Forcing the extra condition $\hat{\Theta}_2'(1) = 0$ results in a relation between Pe_0 and Ge , namely

$$\text{Pe}_0 = 2 \sqrt{\frac{105 \text{Ge}^2}{(20 - \text{Ge}^2) \sqrt{15(15 - \text{Ge}^2)} + 25 \text{Ge}^2 - 300}}. \quad (37)$$

A characteristic feature of equation (37) is that $\text{Pe}_0 \sim \mathcal{O}(\text{Ge}^{-2})$ in the limit $\text{Ge} \rightarrow 0$. This feature justifies our statement in Section VB1 that the ordinate axis $k = 0$ is a vertical asymptote for the neutral stability curve when $\text{Ge} \rightarrow 0$. Equation (37) provides also a rigorous evaluation of the critical Péclet number in the maximum- Ge case, *i.e.*, for $\text{Ge} = \sqrt{15}$. In fact, $k_c = 0$ in this case and

$$\text{Pe}_c = \text{Pe}_0 = 2\sqrt{21} \approx 9.16515. \quad (38)$$

By comparing this result with the numerical value of Pe along the neutral stability curve (see Fig. 5) with $k = 0.01$, we estimate a relative discrepancy less than 0.01%. Such a discrepancy is extremely satisfactory, given that the numerical shooting-method solver employed for the eigenvalue problem (27) yields the smallest accuracy when k is close to 0.

By considering the system obtained from equations (27) to fourth order in k , one obtains

$$\hat{W}_4'''' - 2\hat{W}_2'' - \hat{\Theta}_2 = 0, \quad (39a)$$

$$\hat{\Theta}_4'' - \hat{\Theta}_2 - \left(\text{Pe}_0^2 \hat{W}_4 + 2 \text{Pe}_0 \text{Pe}_2 \hat{W}_2 \right) G'(z) = 0, \quad (39b)$$

$$\begin{aligned} \hat{W}_4(0) = 0, \quad \hat{W}_4'(0) = 0, \quad \hat{\Theta}_4(0) = 0, \quad \hat{\Theta}_4'(0) = 0, \\ \hat{W}_4(1) = 0, \quad \hat{W}_4'(1) = 0. \end{aligned} \quad (39c)$$

The extra condition $\hat{\Theta}_4'(1) = 0$ yields a relation between Pe_2 and Ge . We do not report the analytical expression of Pe_2 , but we just note that it can be used to detect the threshold for k_c to change from zero to nonzero as Ge increases. We already pointed out that the neutral stability curve for longitudinal modes with $\text{Ge} = 2$ has $k_c \neq 0$, while that for $\text{Ge} = \sqrt{15}$ has $k_c = 0$. The threshold value of Ge where k_c changes from a nonzero to a zero value can be detected as that value corresponding to a change in the concavity of the neutral stability curve

Ge	k_c	Pe_c	\mathcal{R}_c	Pe_0	\mathcal{R}_0
0	2.88872	∞	41.8534	∞	∞
0.01	2.88237	417.4493	41.7449	3549.6464	354.9646
0.1	2.82398	128.9560	40.7795	354.9500	112.2450
0.2	2.75634	88.8359	39.7286	177.4528	79.3593
0.3	2.68571	70.6563	38.7001	118.2772	64.7831
0.4	2.61199	59.5981	37.6932	88.6819	56.0874
0.5	2.53508	51.9123	36.7076	70.9188	50.1472
0.8	2.28435	37.8763	33.8776	44.2515	39.5797
1	2.09952	32.0986	32.0986	35.3470	35.3470
1.2	1.89924	27.7601	30.4097	29.4002	32.2063
1.5	1.56474	22.9062	28.0543	23.4372	28.7045
1.8	1.17077	19.3205	25.9212	19.4448	26.0879
2	0.84224	17.4116	24.6237	17.4397	24.6634
2.2	0.31397	15.7919	23.4232	15.7924	23.4239
2.23397	0	15.5412	23.2286	15.5412	23.2286
$\sqrt{15}$	0	9.1652	18.0369	9.1652	18.0369

TABLE I. Values of k_c , Pe_c , \mathcal{R}_c , Pe_0 , \mathcal{R}_0 versus Ge

at $k = 0$. Such a change in concavity corresponds to a change of sign for Pe_2 . In fact, the condition $\text{Pe}_2 = 0$ yields

$$\text{Ge} = 2.23397. \quad (40)$$

3. The Neutral Stability Curves and the Critical Values

The neutral stability curves for longitudinal modes represented in the (k, \mathcal{R}) plane are reported in Fig. 9 for decreasing values of Ge ranging from its maximum, $\sqrt{15}$, to 0.01. The neutral stability curve for the asymptotic case $\text{Ge} \rightarrow 0$ (dashed line) is reported for comparison. The first impression is that the neutral stability curve for $\text{Ge} = 0.01$ matches almost perfectly that for $\text{Ge} \rightarrow 0$. However, by employing equation (37), one should keep in mind that the neutral stability curve for $\text{Ge} = 0.01$ yields a finite, though very large, value of \mathcal{R} in the limit $k \rightarrow 0$, *i.e.* $\mathcal{R} = 354.967$, while the neutral stability curve for the asymptotic case $\text{Ge} \rightarrow 0$ has a vertical asymptote at $k = 0$.

Figure 10 displays a comparison between the critical value of \mathcal{R} and the $k \rightarrow 0$ limiting value of \mathcal{R} versus Ge . In fact, for a given Ge , we define

$$\mathcal{R}_c = \text{Pe}_c \sqrt{\text{Ge}}, \quad \mathcal{R}_0 = \text{Pe}_0 \sqrt{\text{Ge}}. \quad (41)$$

A dark grey line is employed for \mathcal{R}_c and a light grey line for \mathcal{R}_0 . The latter line almost overlaps the former when Ge is greater than 2, while the exact overlapping occurs when Ge exceeds the threshold value given by equation (40) and identified in Fig. 10 by a black dot. The reason is that the difference between \mathcal{R}_c and \mathcal{R}_0 becomes very small when Ge is so large. When $\text{Ge} \rightarrow 0$, the value of \mathcal{R}_c agrees with that given by equation (32). When $\text{Ge} = \sqrt{15} \approx 3.87298$, both the lines come to an end as this value of Ge is the maximum possible for the existence of the basic state. Although hardly significant for

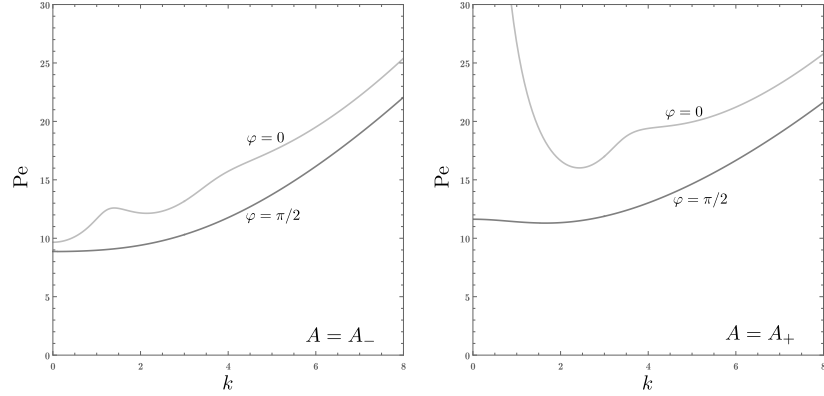


FIG. 11. Neutral stability curves for $Ge = 3.8$ in the (k, Pe) plane for transverse (light grey line, $\varphi = 0$) and longitudinal (dark grey line, $\varphi = \pi/2$) modes. Both dual branches $A = A_-$ and $A = A_+$ are considered

a physical system, the range of Ge very close to its maximum shows a diversion from the general decreasing trend of both \mathcal{R}_c and \mathcal{R}_0 versus Ge with a minimum which can be accurately evaluated for \mathcal{R}_0 by using equation (37),

$$\begin{aligned}\mathcal{R}_{0,\min} &= 3\sqrt{21\sqrt{\frac{5}{2}}} \approx 17.2869, \\ \text{Ge}_{\min} &= 6\sqrt{\frac{2}{5}} \approx 3.79473.\end{aligned}\quad (42)$$

Table I reports the critical data for the parameters k , Pe and \mathcal{R} for several Gebhart numbers, together with the corresponding values of Pe and \mathcal{R} obtained by employing the $k \rightarrow 0$ asymptotic solution equation (37). The first row of this table, for $Ge = 0$, is relative to the asymptotic solution discussed in Section VB1. We note that the discrepancy between the asymptotic case $Ge \rightarrow 0$ and the case $Ge = 0.01$ is less than 0.3% both in terms of k_c and \mathcal{R}_c . This means that, for practical purposes, the asymptotic solution for $Ge \rightarrow 0$ can be safely employed for all cases with $Ge \leq 0.01$. In Table I, we also reported the threshold value of Ge defined by equation (40) above which $k_c = 0$.

Even if we declared that the focus of our stability analysis is on the $A = A_-$ branch, a sample comparison between the stability characteristics of dual flows for a given Gebhart number could be interesting. Thus, we have selected a case, $Ge = 3.8$, very close to the maximum, $Ge = \sqrt{15}$, so that the dual branches are not too different. We recall that the basic dual flows for $Ge = 3.8$ are illustrated in Figs. 1 and 3 and commented on in Section III. The neutral stability curves relative to both the dual branches with $Ge = 3.8$ are displayed in Fig. 11 for transverse modes and for longitudinal modes. In both dual branches, the longitudinal modes are the most unstable. However, the $A = A_-$ branch displays a critical

value of Pe smaller than the critical value for the $A = A_+$ branch. Then, the $A = A_-$ is more unstable than the $A = A_+$ branch in this case. This outcome is not surprising as a similar behaviour was observed in a similar previous studies dealing with Darcy's flow in a porous channel²¹. A minor aspect clearly visible in Fig. 11 is that the onset of instability with longitudinal modes, for the $A = A_+$ branch, happens with a nonzero wavenumber mode. On the other hand, $k_c = 0$ for the $A = A_-$ branch.

VI. CONCLUSIONS

The onset of convective instability for the buoyant parallel flows in a horizontal plane channel with adiabatic walls has been studied. The action of buoyancy and the unstable behaviour are induced by the viscous dissipation for a flow with a given mass flow rate.

The main features and, in particular, the duality of the basic parallel flows have been surveyed. The stability analysis has been focussed on the lower branch of the dual flows, as the higher branch turned out to display features utterly incompatible with the Oberbeck-Boussinesq approximation. The governing dimensionless parameters for the dual flows are the Gebhart number, Ge , also known as the dissipation number, and the Péclet number, Pe .

The stability analysis has been formulated by evaluating the neutrally stable value of Pe for a given Ge . Since the dual flows are mathematically defined only with $Ge \leq \sqrt{15}$, this whole parametric range has been explored. However, it has been also mentioned that values of Ge as large as its maximum are hardly significant for any real-world application, even over length scales of geophysical interest Barletta, Celli, and Brandão¹⁸.

The linear stability analysis has been formulated by assuming creeping flow, which means an infinite Prandtl number. Such an analysis has been carried out through a numerical solution of the stability eigenvalue problem obtained by the shooting method. The main results of the stability analysis can be summarised as follows:

- The preferred perturbation modes causing the transition to instability are longitudinal, for every value of Ge . The reaction of the base flows to arbitrary oblique perturbation modes has been tested by defining the inclination angle φ between the base flow direction and the wave vector corresponding to the oblique modes. Then, the inclination angle has been varied in the range $0 \leq \varphi \leq \pi/2$, with $\varphi = 0$ identifying the transverse modes and $\varphi = \pi/2$ defining the longitudinal modes. The value $\varphi = \pi/2$ always yields the least stable condition.
- The analysis of the neutral stability condition for the longitudinal modes reveals that such modes are non-travelling as their angular frequency and, hence, their phase velocity is always zero. The critical values of either Pe or the parameter $\mathcal{R} = Pe\sqrt{Ge}$ are generally decreasing functions of Ge , except for a very narrow range close to the maximum $Ge = \sqrt{15}$. The longitudinal modes with a zero wavenumber, or an infinite wavelength, have a finite neutrally stable value of Pe for any nonzero Ge . This regime has been studied via an analytical asymptotic solution.
- A physically important situation is one where Ge is negligibly small, the Péclet number is very large, but the parameter \mathcal{R} remains finite. For this limiting case, the critical condition for the onset of the instability has been evaluated as $\mathcal{R}_c = 41.8534$.

The study of the instability induced by the viscous dissipation has been carried out in this paper by assuming conditions of creeping flow where the Prandtl number is prescribed to be extremely large though maintaining a finite Péclet number. With this scenario in mind, the viscous dissipation instability is one emerging at very small Reynolds numbers and, hence, has likely no interrelation with the hydrodynamic instability analysed through the solution of the Orr-Sommerfeld problem. The extension of our study to a hybrid parametric domain where a finite Prandtl number is assumed can be a challenge for future investigations. Such a development can offer a chance to test the interplay between the viscous dissipation instability and the Orr-Sommerfeld hydrodynamic instability in a plane parallel channel.

Acknowledgement

The authors acknowledge financial support from Italian Ministry of Education, University and Research (MIUR) grant number PRIN 2017F7KZWS.

Data Availability Statement

The data that supports the findings of this study are available within the article.

Conflict of Interest Statement

The authors have no conflicts to disclose.

Author Contributions

All authors contributed equally with their work to the conceptualisation, formal analysis, investigation, validation and writing of this paper.

REFERENCES

- ¹P. G. Drazin and W. H. Reid, *Hydrodynamic Stability*, 2nd ed. (Cambridge University Press, 2004).
- ²P. K. Kundu, I. M. Cohen, and D. R. Dowling, *Fluid Mechanics*, 6th ed. (Academic Press, 2016).
- ³D. D. Joseph, "Variable viscosity effects on the flow and stability of flow in channels and pipes," *The Physics of Fluids* **7**, 1761–1771 (1964).
- ⁴D. D. Joseph, "Stability of frictionally-heated flow," *The Physics of Fluids* **8**, 2195–2200 (1965).
- ⁵A. Barletta and D. A. Nield, "Convection-dissipation instability in the horizontal plane Couette flow of a highly viscous fluid," *Journal of Fluid Mechanics* **662**, 475–492 (2010).
- ⁶A. Barletta, M. Celli, and D. A. Nield, "On the onset of dissipation thermal instability for the Poiseuille flow of a highly viscous fluid in a horizontal channel," *Journal of Fluid Mechanics* **681**, 499–514 (2011).
- ⁷A. Barletta, "On the thermal instability induced by viscous dissipation," *International Journal of Thermal Sciences* **88**, 238–247 (2015).
- ⁸M. Miklavčič, "Stability analysis of some fully developed mixed convection flows in a vertical channel," *ZAMM-Journal of Applied Mathematics and Mechanics/Zeitschrift für Angewandte Mathematik und Mechanik* **95**, 982–986 (2015).
- ⁹A. Barletta and M. Miklavčič, "On fully developed mixed convection with viscous dissipation in a vertical channel and its stability," *ZAMM-Journal of Applied Mathematics and Mechanics/Zeitschrift für Angewandte Mathematik und Mechanik* **96**, 1457–1466 (2016).
- ¹⁰L. A. Lund, Z. Omar, I. Khan, S. Kadry, S. Rho, I. A. Mari, and K. S. Nisar, "Effect of viscous dissipation in heat transfer of MHD flow of micropolar fluid partial slip conditions: dual solutions and stability analysis," *Energies* **12**, 4617 (2019).
- ¹¹Y. Requilé, S. C. Hirata, M. N. Ouarzazi, and A. Barletta, "Weakly nonlinear analysis of viscous dissipation thermal instability in plane Poiseuille and plane Couette flows," *Journal of Fluid Mechanics* **886** (2020).
- ¹²L. A. Lund, Z. Omar, J. Raza, and I. Khan, "Magnetohydrodynamic flow of Cu-Fe₃O₄/H₂O hybrid nanofluid with effect of viscous dissipation: dual similarity solutions," *Journal of Thermal Analysis and Calorimetry* **143**, 915–927 (2021).
- ¹³E. V. M. Reis and L. S. de B. Alves, "Convective and absolute instabilities induced by viscous dissipation in the thermocapillary convection with through-flow," *ASME Journal of Heat Transfer* **143**, 052601 (2021).
- ¹⁴A. Barletta and G. Mulone, "The energy method analysis of the Darcy-Bénard problem with viscous dissipation," *Continuum Mechanics and Thermodynamics* **33**, 25–33 (2021).

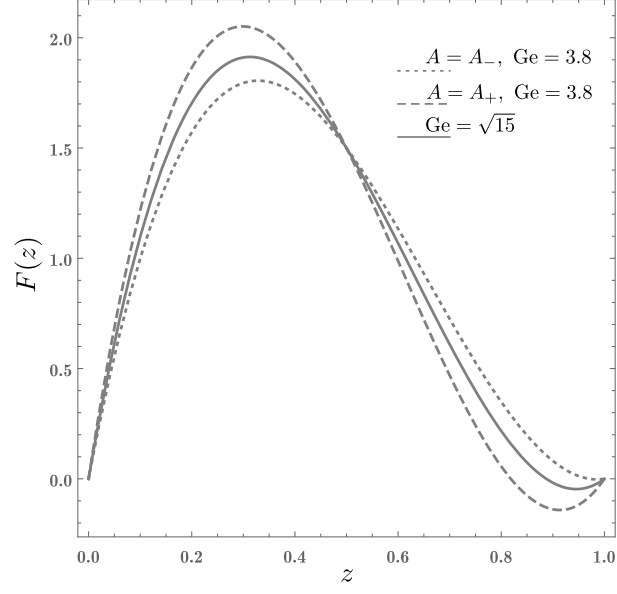
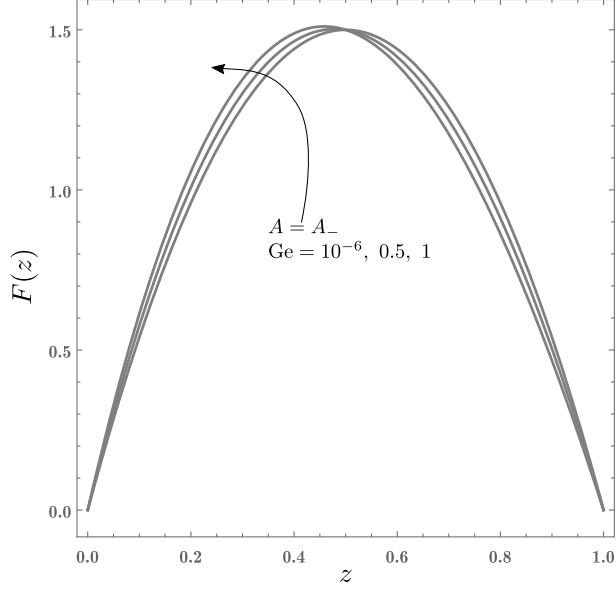
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878

- ¹⁵K. Ali Amar, S. C. Hirata, and M. N. Ouarzazi, "Soret effect on the onset of viscous dissipation thermal instability for Poiseuille flows in binary mixtures," *Physics of Fluids* **34**, 114101 (2022).
- ¹⁶D. L. Turcotte, D. A. Spence, and H. H. Bau, "Multiple solutions for natural convective flows in an internally heated, vertical channel with viscous dissipation and pressure work," *International Journal of Heat and Mass Transfer* **25**, 699–706 (1982).
- ¹⁷A. Barletta, E. Magyari, and B. Keller, "Dual mixed convection flows in a vertical channel," *International Journal of Heat and Mass Transfer* **48**, 4835–4845 (2005).
- ¹⁸A. Barletta, M. Celli, and P. V. Brandão, "On mixed convection in a horizontal channel, viscous dissipation and flow duality," *Fluids* **7**, 170 (2022).
- ¹⁹G. Wilks and J. S. Bramley, "Dual solutions in mixed convection," *Proceedings of the Royal Society of Edinburgh: Section A Mathematics* **87**, 349–358 (1981).
- ²⁰K. Naganthran, M. Mustafa, A. Mushtaq, and R. Nazar, "Dual solutions for fluid flow over a stretching/shrinking rotating disk subject to variable fluid properties," *Physica A: Statistical Mechanics and Its Applications* **556**, 124773 (2020).
- ²¹A. Barletta and D. A. S. Rees, "Stability analysis of dual adiabatic flows in a horizontal porous layer," *International Journal of Heat and Mass Transfer* **52**, 2300–2310 (2009).
- ²²B. Gebhart, "Effects of viscous dissipation in natural convection," *Journal of Fluid Mechanics* **14**, 225–232 (1962).
- ²³C. Kincaid and P. Silver, "The role of viscous dissipation in the orogenic process," *Earth and Planetary Science Letters* **142**, 271–288 (1996).
- ²⁴A. P. van den Berg and D. A. Yuen, "The role of shear heating in lubricating mantle flow," *Earth and planetary science letters* **151**, 33–42 (1997).
- ²⁵B. Straughan, *The Energy Method, Stability, and Nonlinear Convection* (Springer, 2013).
- ²⁶A. Barletta, *Routes to Absolute Instability in Porous Media* (Springer, 2019).
- ²⁷H. Park and L. Sirovich, "Hydrodynamic stability of Rayleigh-Bénard convection with constant heat flux boundary condition," *Quarterly of Applied Mathematics* **49**, 313–332 (1991).

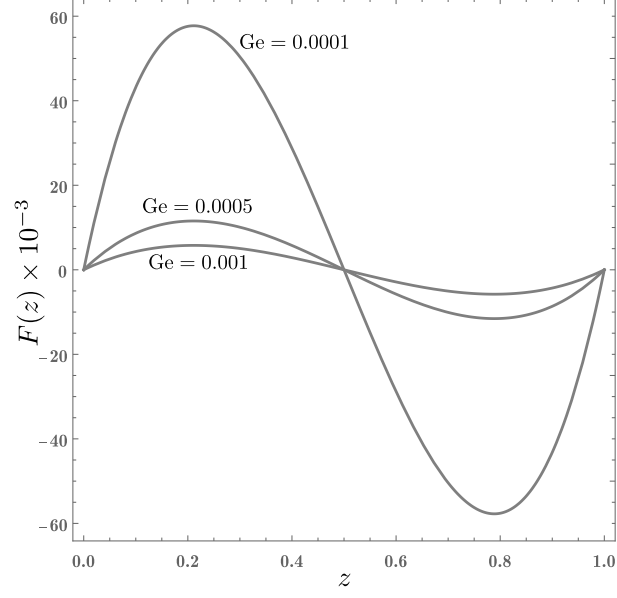
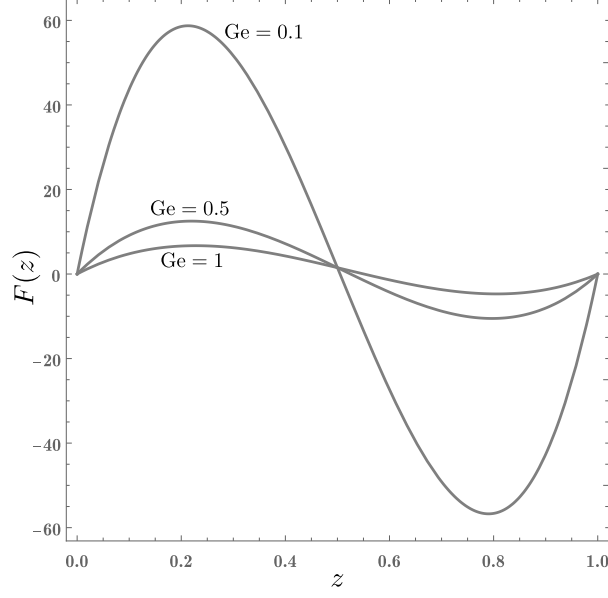
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



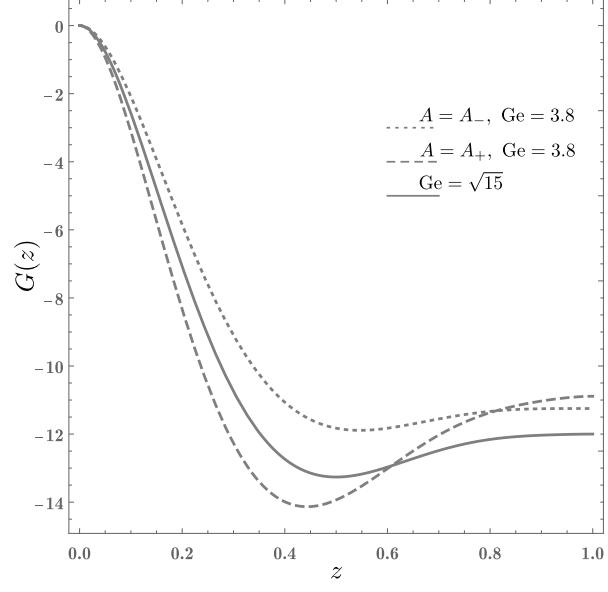
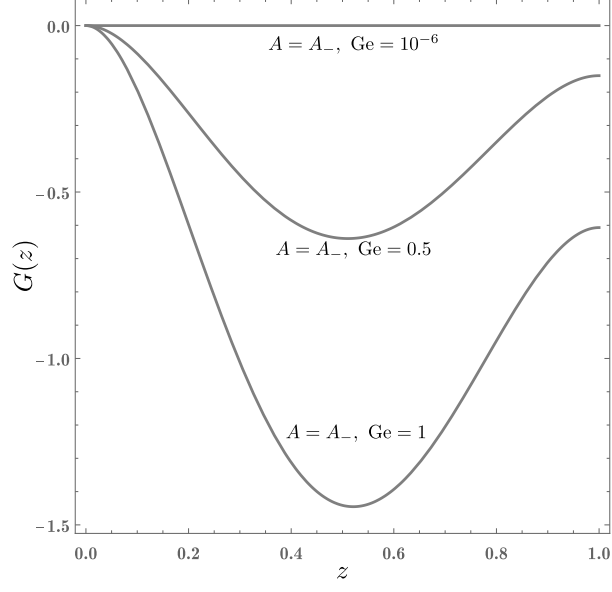
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



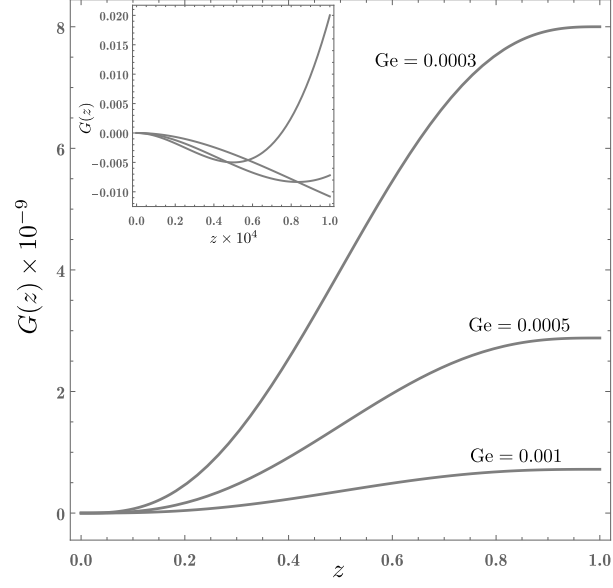
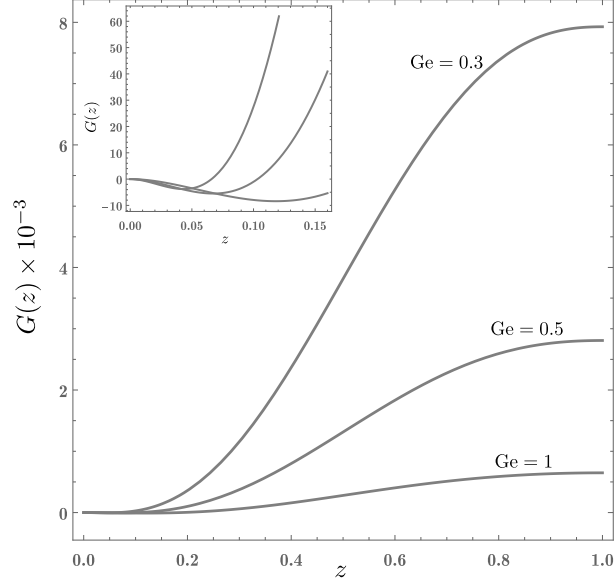
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



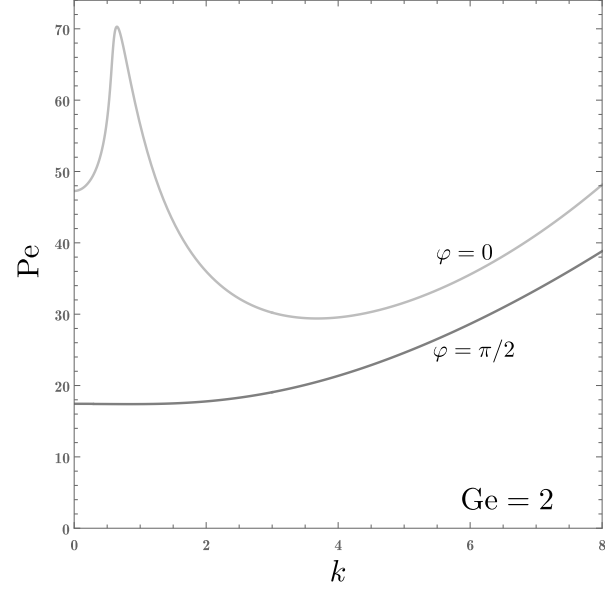
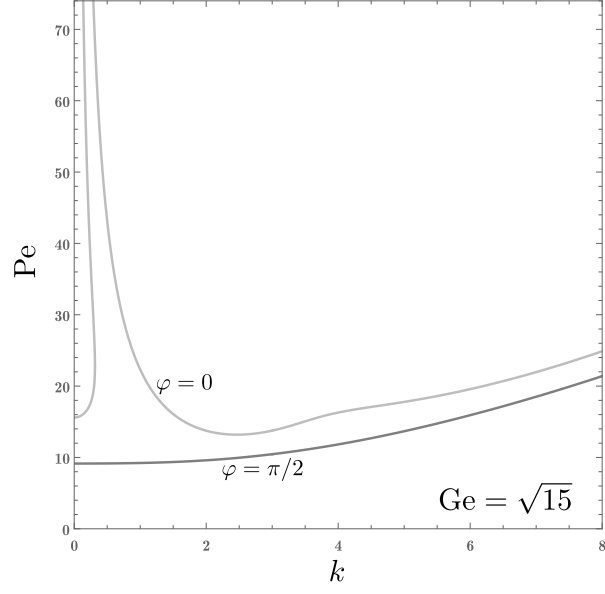
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



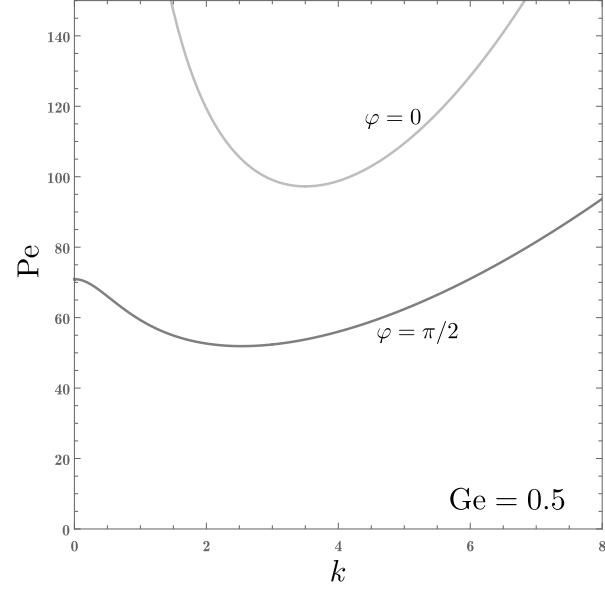
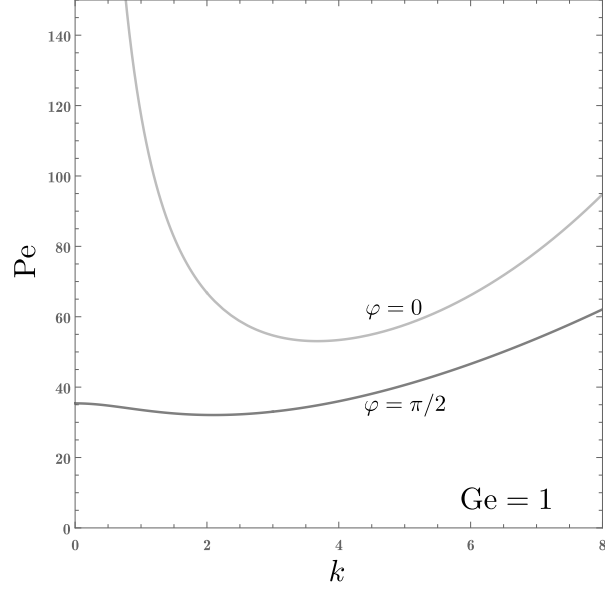
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



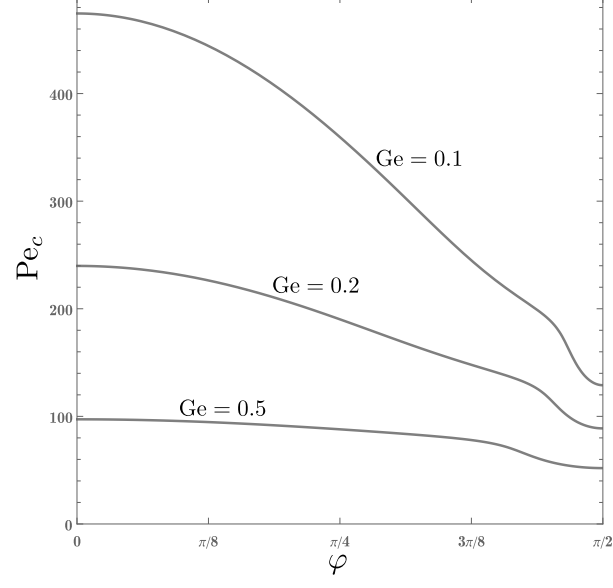
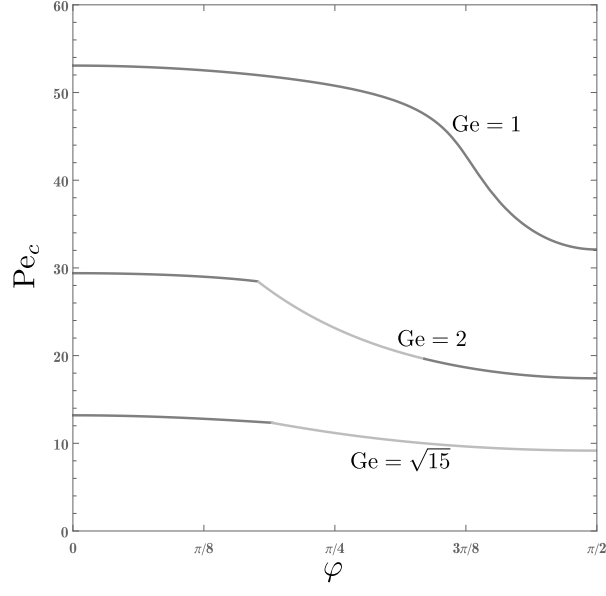
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



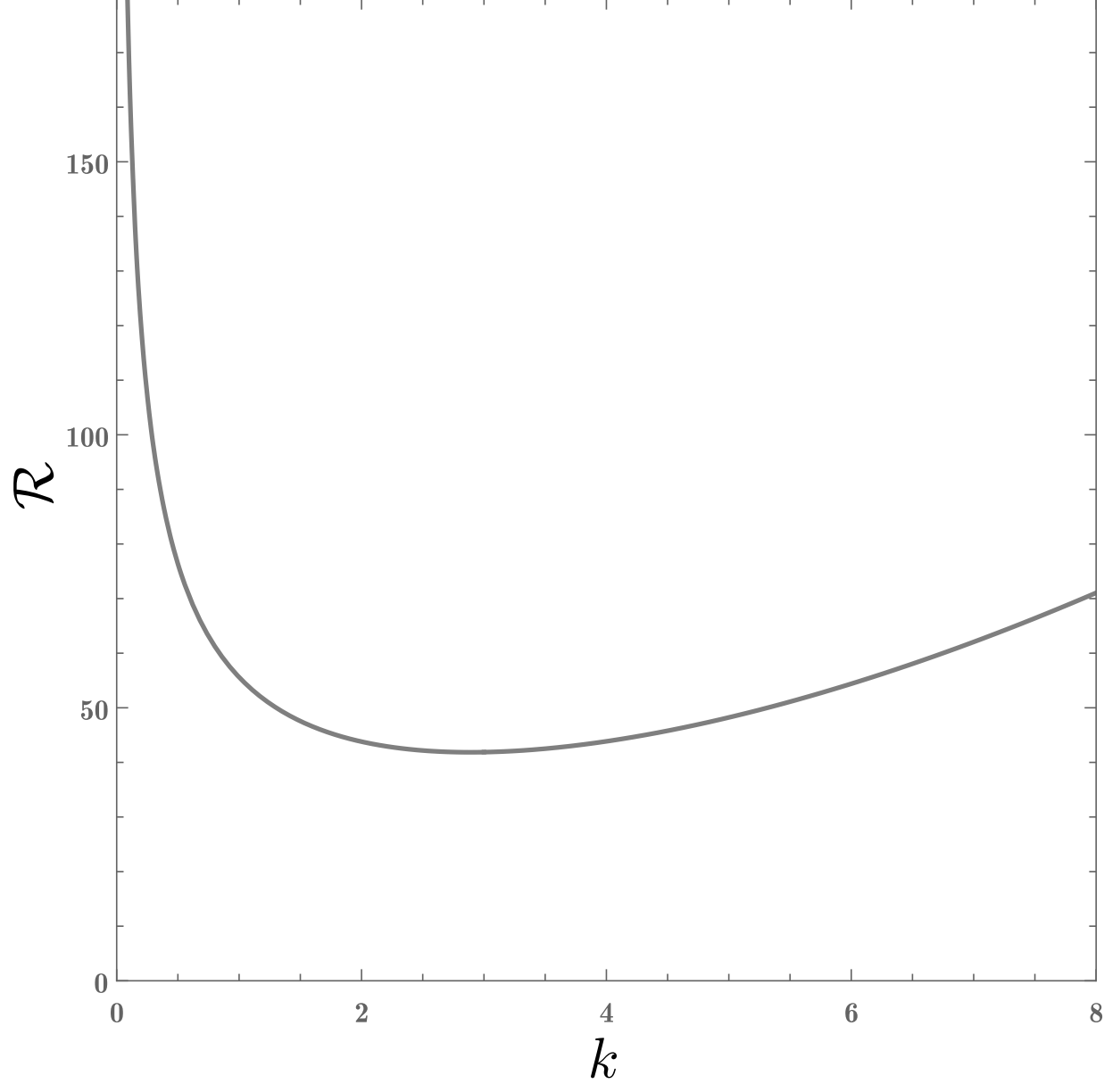
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



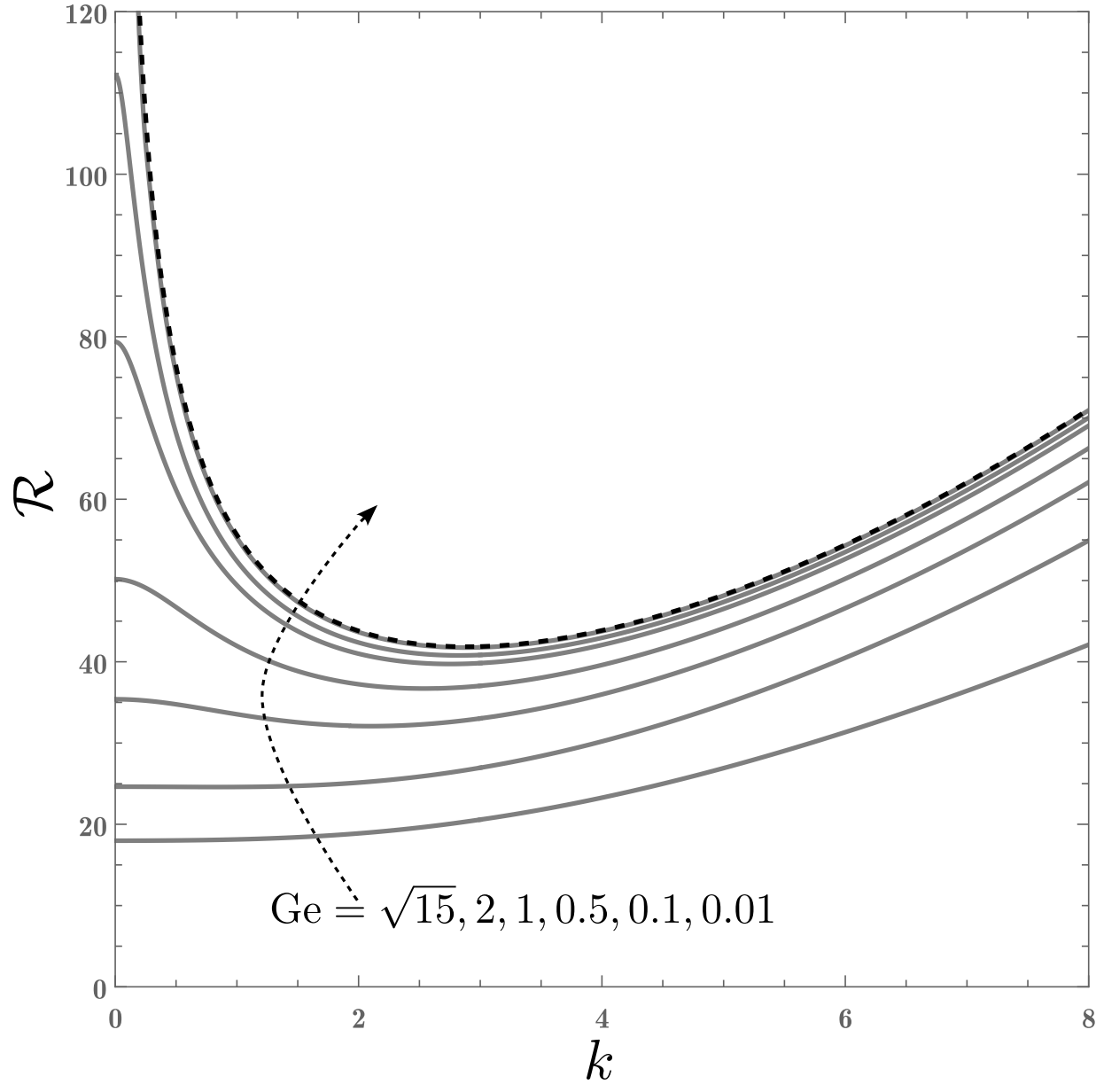
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



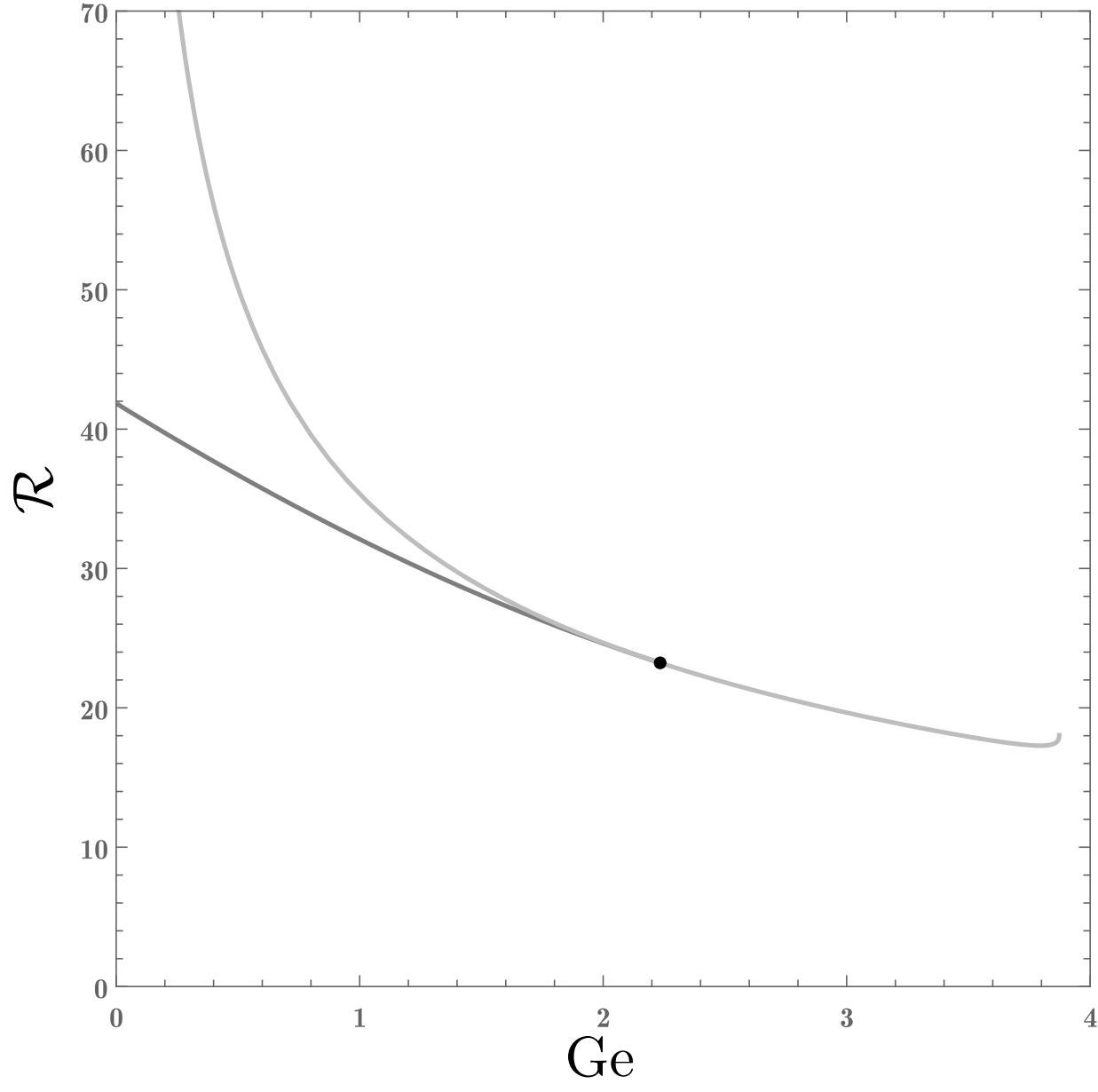
This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878



This is the author's peer reviewed, accepted manuscript. However, the online version of record will be different from this version once it has been copyedited and typeset.

PLEASE CITE THIS ARTICLE AS DOI: 10.1063/5.0144878

